

Chemical Looping Combustion for inherent CO₂ capture in a coal-based IGCC power plant

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Presentation to the
2011 AIChE Spring Meeting, Chicago, IL
March 13-17, 2011

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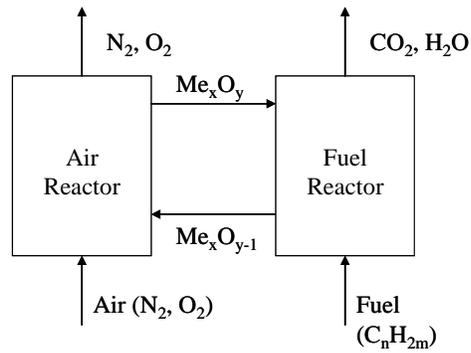
Objectives

- Evaluate CLC using syngas as fuel
 - Effect of fuel
 - Effect of operating conditions
- Use CLC for CO₂-capture in a coal-based IGCC power plant using different gasification technologies

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What is CLC

- Indirect combustion process
- Produces a high purity CO₂ stream
- Oxygen supplied by an oxygen carrier
- Possible OC
 - Ni
 - Cu
 - Fe
 - Mn



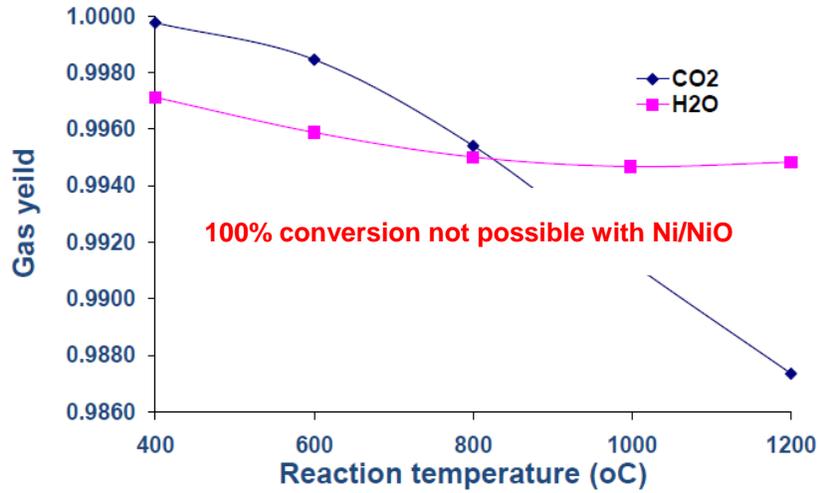
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Reactions

- $\text{Ni} + \frac{1}{2} \text{O}_2 \rightleftharpoons \text{NiO}$
 $\Delta H = -234 \text{ kJ/mol}$
- $\text{CH}_4 + 4\text{NiO} \rightleftharpoons \text{CO}_2 + 2\text{H}_2\text{O} + 4\text{Ni}$
 $\Delta H = 134 \text{ kJ/mol}$
- $\text{CO} + \text{NiO} \rightleftharpoons \text{CO}_2 + \text{Ni}$
 $\Delta H = -43.3 \text{ kJ/mol}$
- $\text{H}_2 + \text{NiO} \rightleftharpoons \text{H}_2\text{O} + \text{Ni}$
 $\Delta H = -2.1 \text{ kJ/mol}$
- $x\text{CO} + y\text{H}_2 + z\text{CH}_4 + (x+y+4z)\text{NiO} \rightleftharpoons (x+z)\text{CO}_2 + (y+2z)\text{H}_2\text{O} + (x+y+4z)\text{Ni}$

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Conversion decreases with temperature

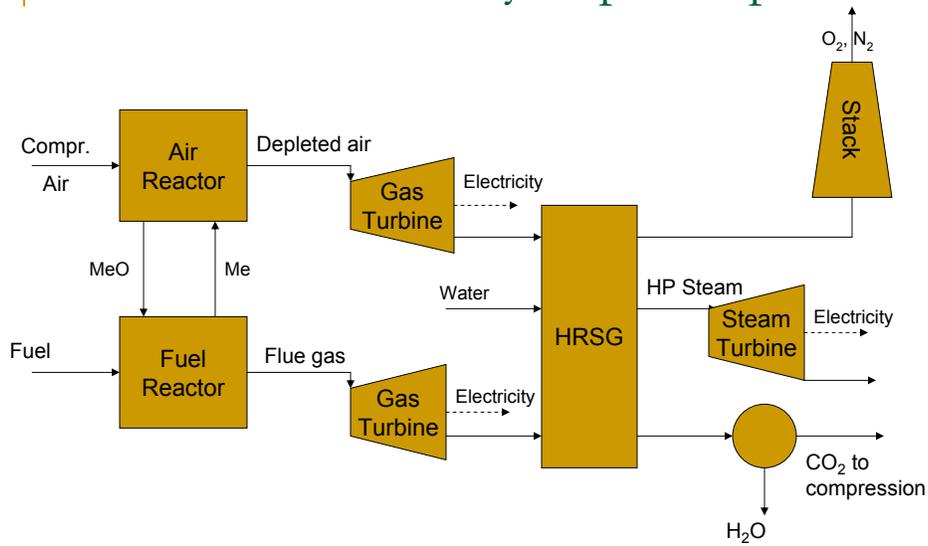


$$\gamma_{CO} = \frac{P_{CO_2}}{P_{CO_2} + P_{CO}}$$

$$\gamma_{H_2} = \frac{P_{H_2O}}{P_{H_2O} + P_{H_2}}$$

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CLC in a combined cycle power plant



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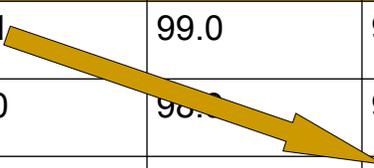
CLC model assumptions

- Fuel
 - 100% CO
 - 75% CO, 25% H₂
 - 50% CO, 50% H₂
- Air reactor (AR) – isothermal, 20 bar
 - 1000°C, 1100°C, 1200°C
- Fuel reactor (FR) – adiabatic, 20 bar
- Stoichiometric MeO
- Air-fuel ratio
 - Stoichiometric – 3*Stoichiometric
- Gas turbine
 - No special changes required for depleted air or CO₂/H₂O expansion
- Steam cycle
 - Heat rate – 8,740 kJ/kWh

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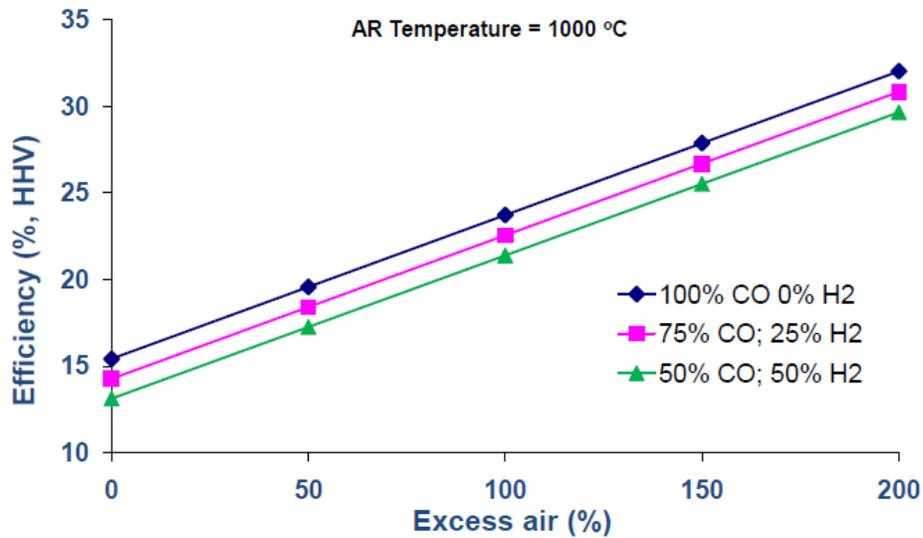
CO₂ purity

Temperature	100% CO	75% CO, 25% H ₂	50% CO, 50% H ₂
1000 °C	99.1	99.0	98.8
1100 °C	99.0	98.9	98.7
1200 °C	98.9	98.8	98.6



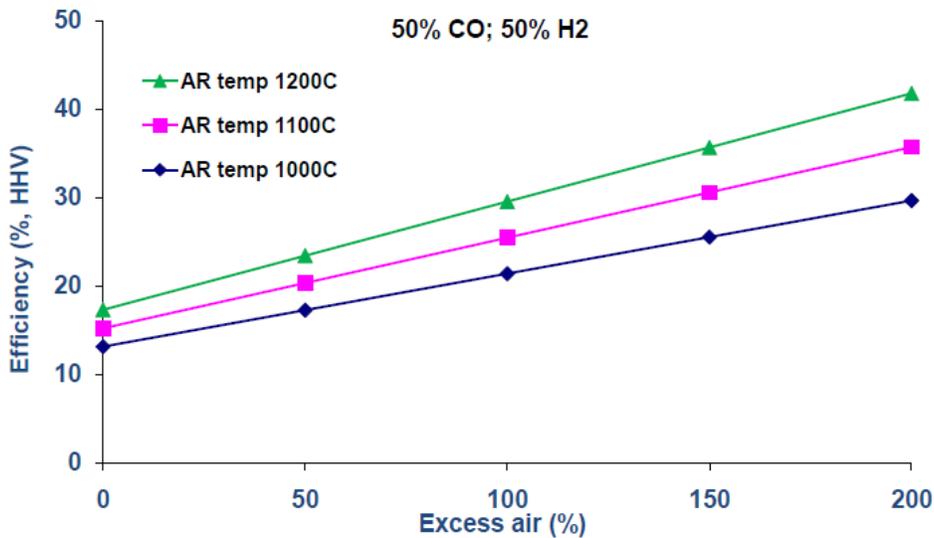
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Efficiency increases with CO%



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Efficiency increases with temperature

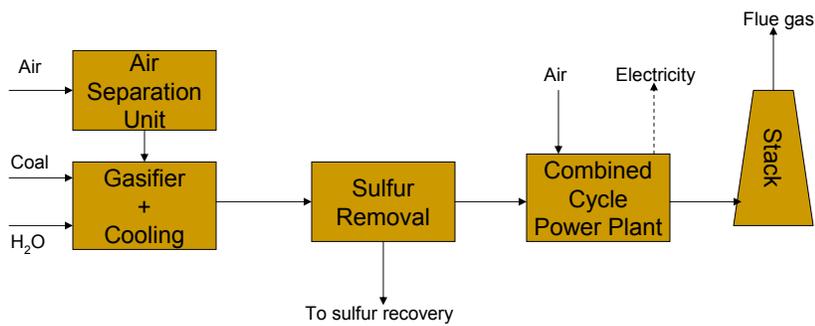


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Application to IGCC

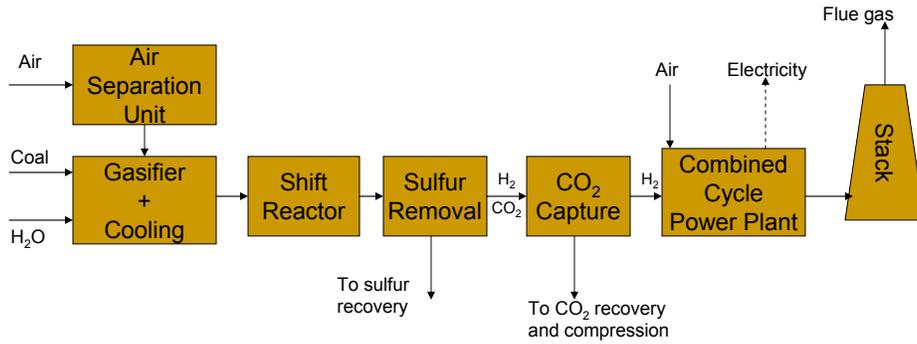
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IGCC without CCS



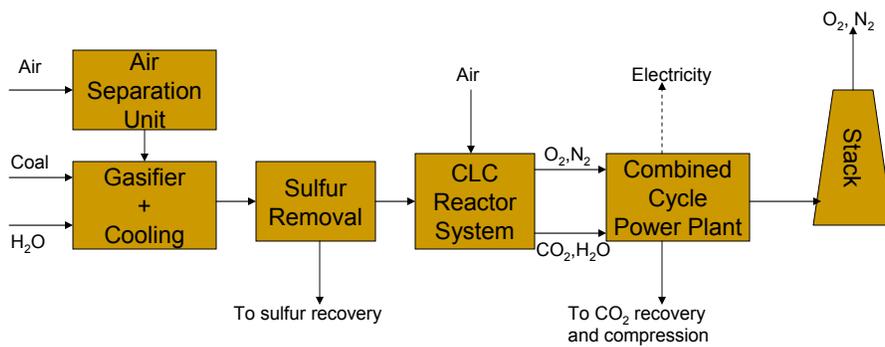
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IGCC with physical absorption CCS



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IGCC with CLC



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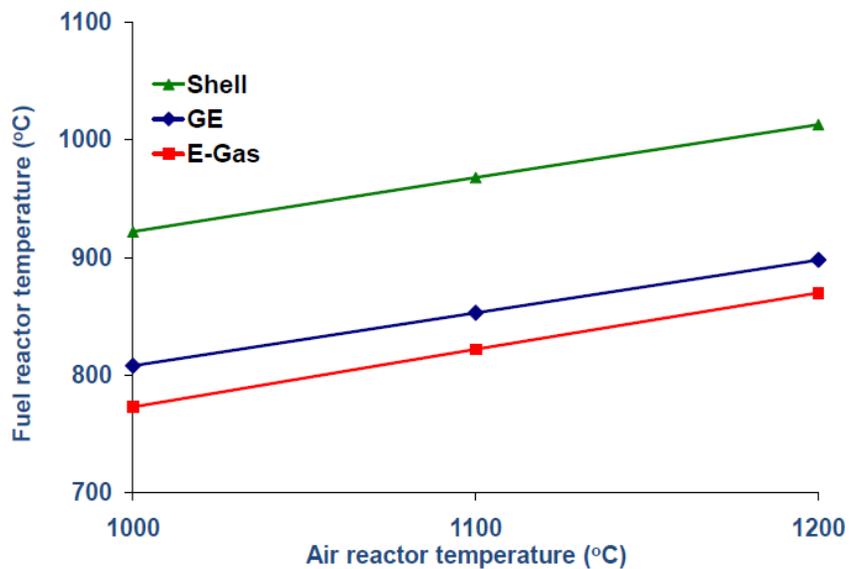
Clean syngas from different gasifiers*

Component	GE (1,316 °C 5.6 MPa)	EGas (1,040 °C 4.2 MPa)	Shell (1,427 °C 4.2 MPa)
CO	38.9	45.4	61.5
H ₂	38.4	32.4	31.2
CH ₄	0.3	4.7	0.0
CO ₂	17.8	15.1	0.1
H ₂ O	0.1	0.2	0.1
N ₂	3.6	1.2	6.0
Ar	0.9	1.0	1.1
MW (kg/kmol)	21	22	20
HHV (kJ/kmol)	222,430	263,200	263,900

* From NETL Baseline Report on Power Plants (2007)

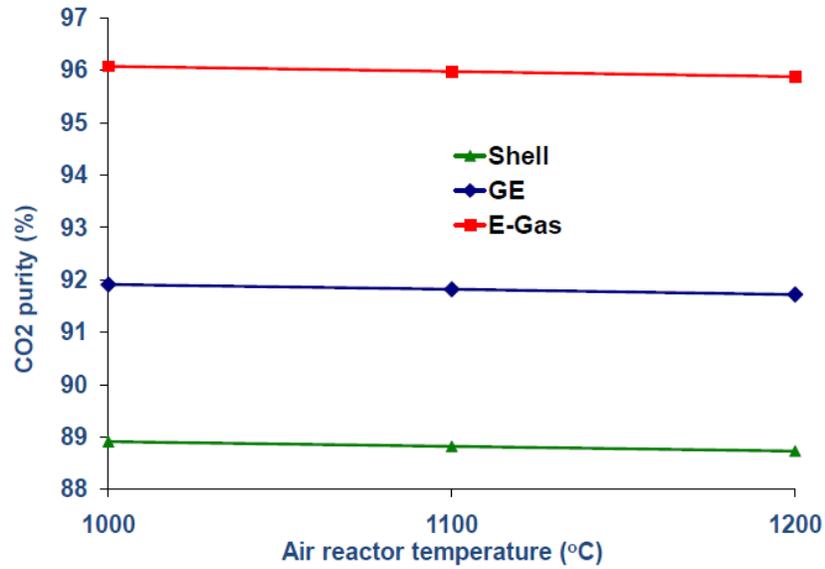
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Fuel reactor temperature



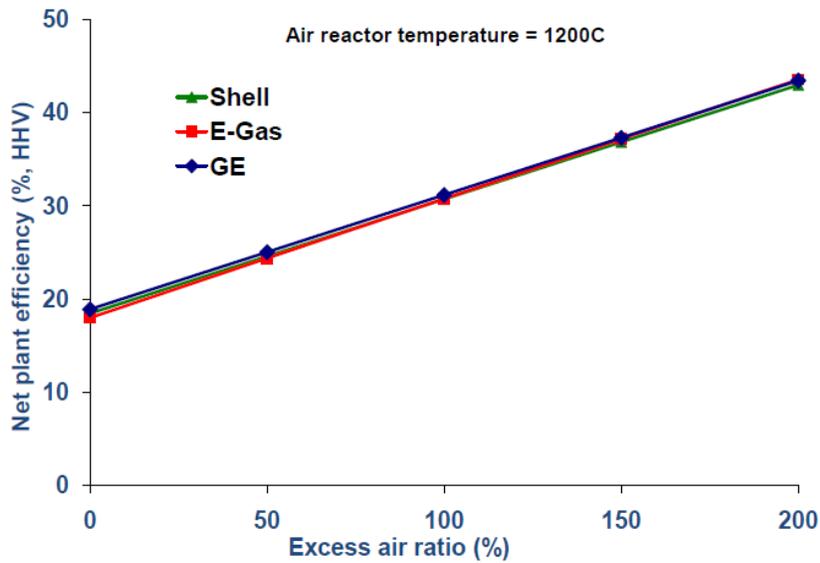
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CO₂ purity



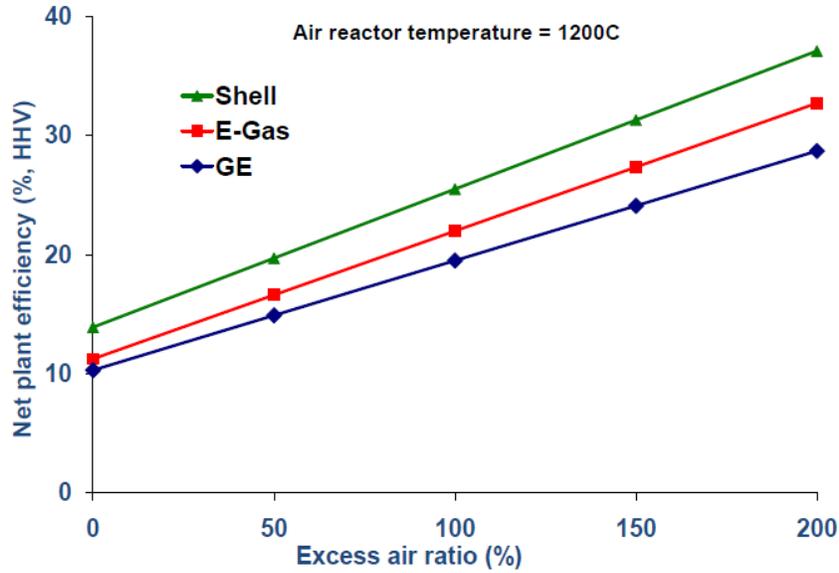
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CLC efficiency for different fuels



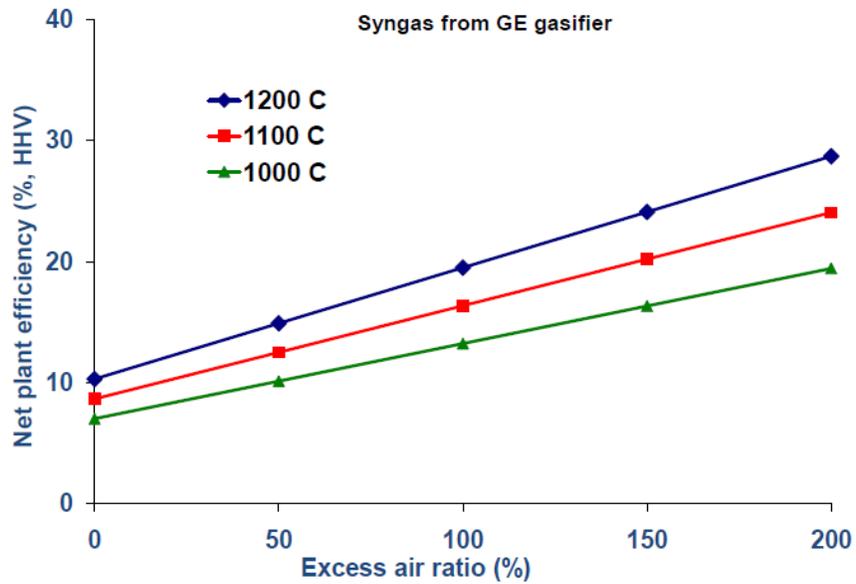
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IGCC efficiency for different fuels

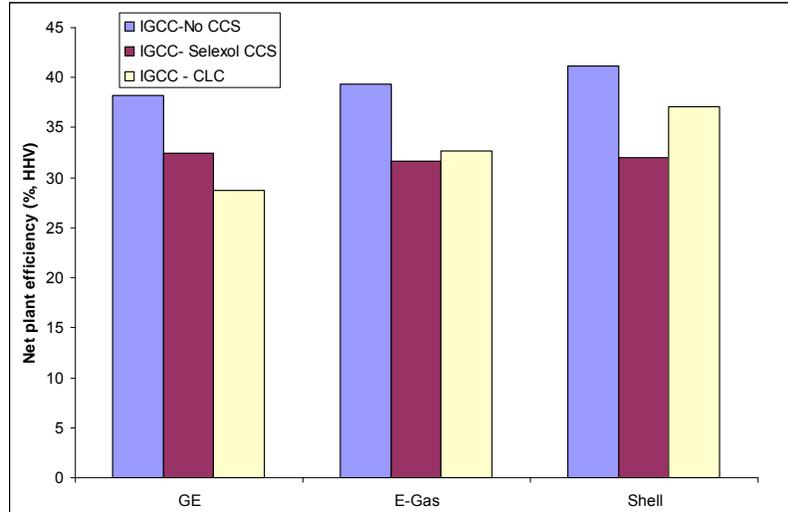


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IGCC efficiency at different temperatures



Comparison with Selexol CCS



Conclusions

- CLC system efficiency doesn't change with fuel
- IGCC system efficiency changes