The Future Cost of Power Plants with CO_2 Capture

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Study Objective

- Develop an empirically-based method to estimate future costs of power plants with CO_2 capture
- Potential applications to large-scale energy-economic modeling, R&D planning, and other related efforts

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- IEA GHG (John Davison)

Use Powerful Analytical Methods

Two Approaches to Estimating Future Technology Costs

- *Method 1:* Engineering-Economic Modeling
  - A "bottom up" approach based on engineering process models, informed by expert elicitations regarding potential improvements in key process parameters
- *Method 2:* Use of Historical Experience Curves
  - A "top down" approach based on use of mathematical "learning curves" or "experience curves" reflecting historical trends for analogous technologies or systems

This study employs the latter method

Study Approach

- Quantify historical learning rates of energy and environmental technologies relevant to power plants with CO_2 capture
- Apply these results to leading plant design options to estimate learning rates and future costs of plant with CO_2 capture*

** This study does not include the costs of CO_2 transport and storage*

- Detailed report available from International Energy Agency Greenhouse Gas Programme (IEA GHG)

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Retrospective Case Studies

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Case Study Technologies

- Flue gas desulfurization systems (FGD)
- Selective catalytic reduction systems (SCR)
- Gas turbine combined cycle system (GTCC)
- Pulverized coal-fired boilers (PC)
- Liquefied natural gas plants (LNG)
- Oxygen production plants (ASU)
- Hydrogen production plants (SMR)

Learning Curve Formulation

General equation:

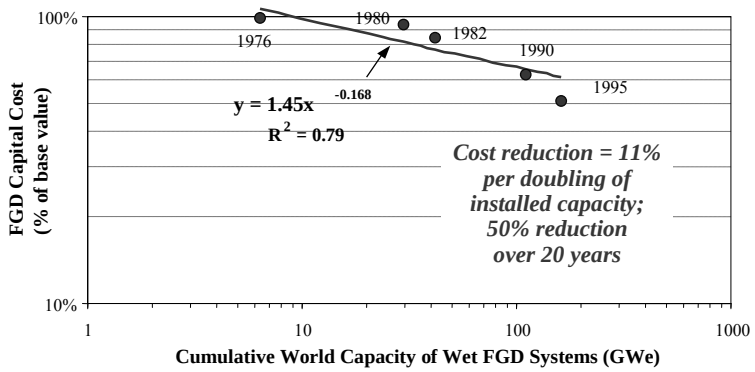
$$y_i = a x_i^{-b}$$

where,

y_i = time or cost to produce i^{th} unit
x_i = cumulative production thru period i
b = learning rate exponent
a = coefficient (constant)

Percent cost reduction for a doubling of cumulative output is called the "learning rate" (LR) = $(1 - 2^{-b})$

FGD System Capital Costs



(Based on 90% SO_2 removal, 500 MW plant, 3.5%S coal)

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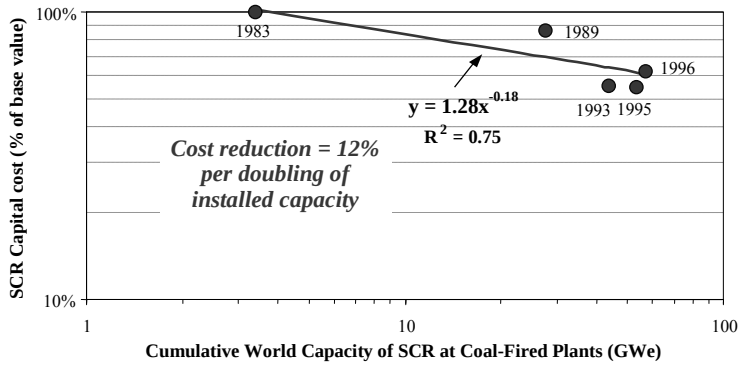
SCR System Capital Costs



(Based on 80% NO_x removal, 500 MW plant, medium S coal)

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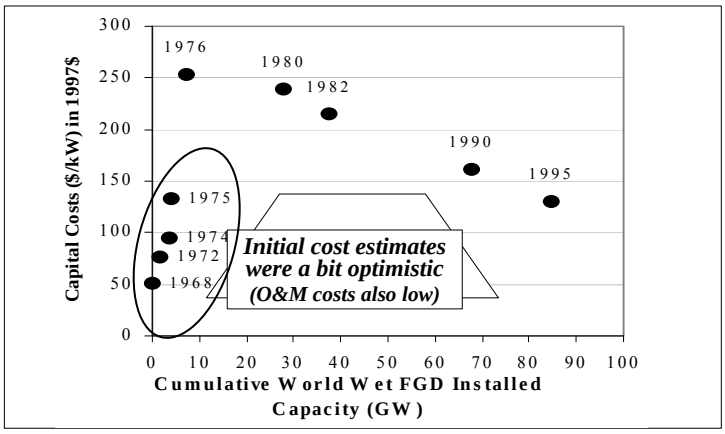
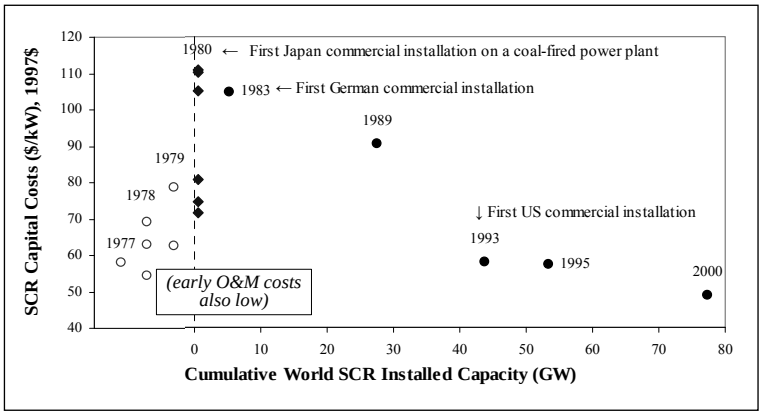
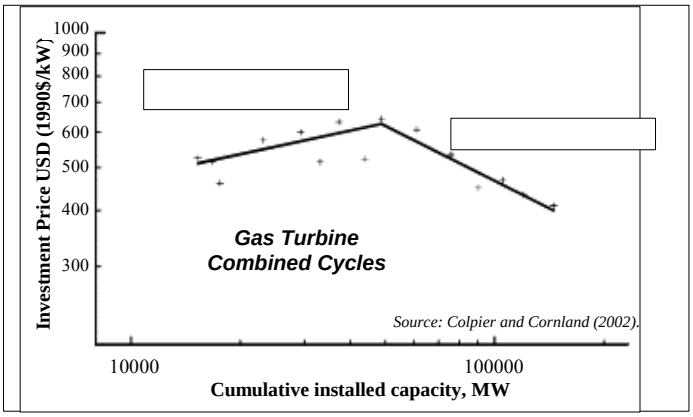
Early Trend of FGD Capital Cost



Early Trend of SCR Cost Estimates



GTCC Capital Costs



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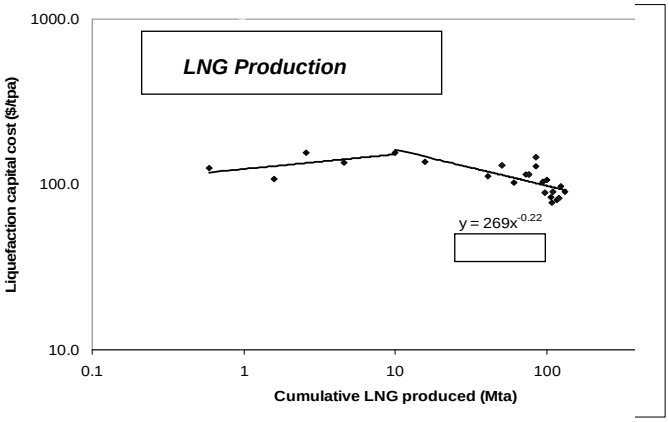
LNG Plant Capital Costs



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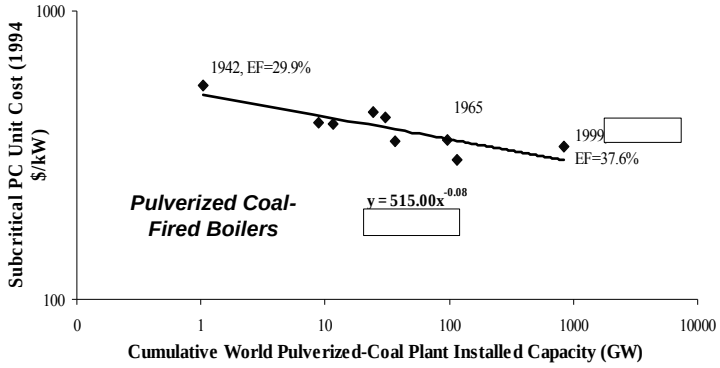
PC Boiler Capital Costs



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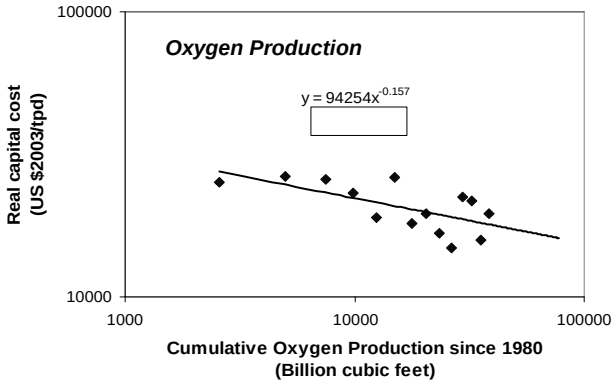
Oxygen Plant Capital Cost



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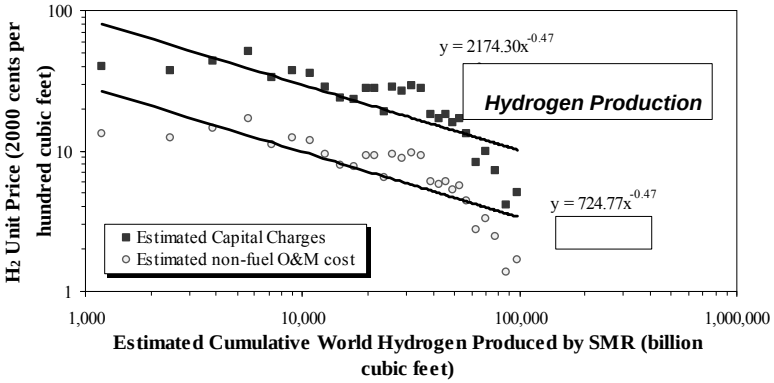
Hydrogen Plant Cost Trends



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Case Study Learning Rates

Technology	"Best Estimate" Learning Rates	
	Capital Cost	O&M Cost
Flue gas desulfurization (FGD)	0.11	0.22
Selective catalytic reduction (SCR)	0.12	0.13
Gas turbine combined cycle (GTCC)	0.10	0.06
Pulverized coal (PC) boilers	0.05	0.18
LNG production	0.14	0.12
Oxygen production (ASU)	0.10	0.05
Hydrogen production (SMR)	0.27	0.27

Results are within ranges reported for other energy-related technologies

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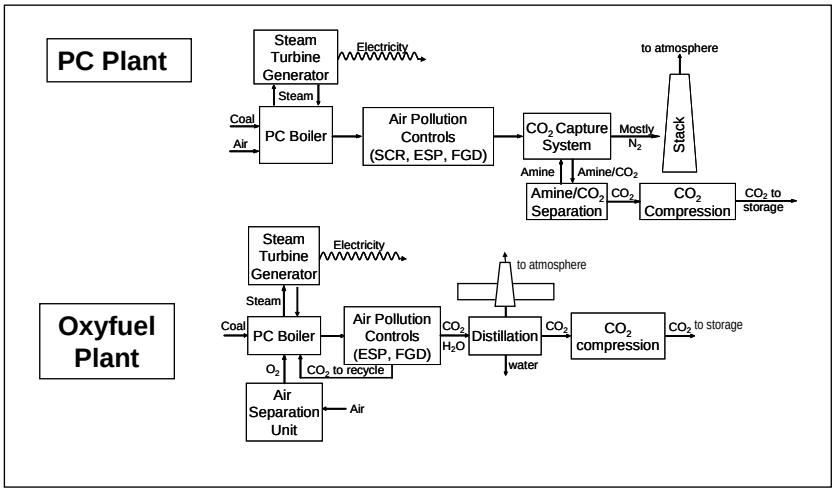
Application to Power Plants with CO_2 Capture

Power Plants with CO_2 Capture

- PC plant with post-combustion capture (amine system)
- NGCC plant with post-combustion capture (amine system)
- IGCC coal plant with pre-combustion capture (WGS + Selexol)
- PC plant with oxyfuel combustion

Baseline Plant Designs *(1)*



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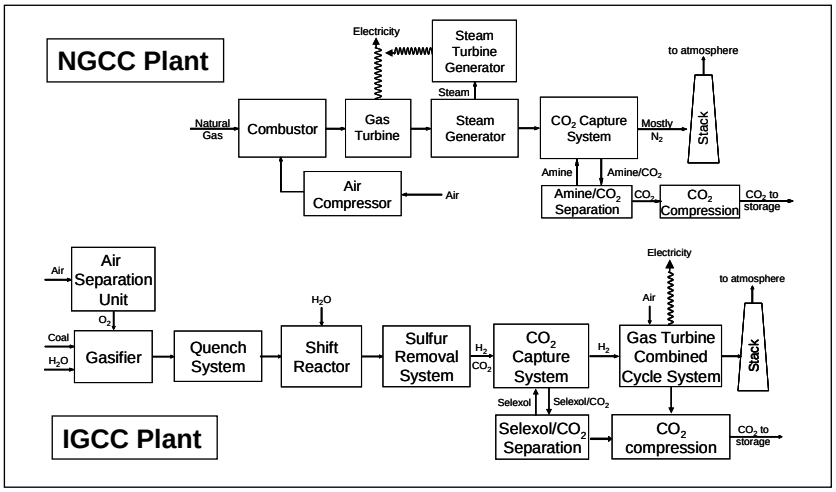
Baseline Plant Designs *(2)*



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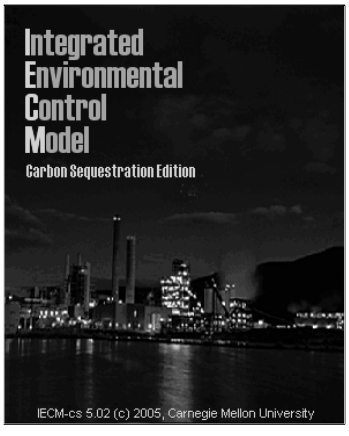
Baseline Plant Characteristics

- Approximately 500 MW net output
- Supercritical PC and Quench gasifier IGCC
- Pittsburgh #8 bituminous coal
- 75% levelized capacity factor
- 14.8% fixed charge factor
- All costs in constant 2002 dollars

Baseline costs obtained from IECM

- **A** computer model developed for DOE/NETL, benchmarked on recent engineering studies
- Provides preliminary design estimates of performance, emissions and cost for:
  - PC, NGCC and IGCC plants
  - Conventional AP controls
  - CCS options (pre- and post-combustion, oxyfuel comb.)
- Free Web Download :
  - www. iecm-online.com



Step 1: Disaggregate each plant into major sub-sections

For example:

- IGCC Plant Components
  - Air separation unit
  - Gasifier area
  - Sulfur removal/recovery system
  - CO_2 capture system (WGS+Selexol)
  - CO_2 compression
  - GTCC (power block)
  - Fuel cost

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Step 2: Estimate current plant costs and contribution of each sub-section

Levelized costs in constant $2002

Plant Type & Technology	Capital Cost	Annual O&M Cost*	Cost of Electricity*
IGCC Plant w/ Capture	**1,831** $/kW	**21.3** $/MWh	**62.6** $/MWh
Air separation unit	18 %	8 %	14 %
Gasifier area	27 %	17 %	24 %
Sulfur removal/recovery	6 %	3 %	5 %
CO_2 capture system*	13 %	7 %	11 %
CO_2 compression	2%	2 %	2 %
GTCC (power block)	34 %	9 %	25 %
Fuel cost**	--	54%	19 %

*Excludes costs of CO_2 transport and storage **Based on Pittsburgh #8 coal @ $1.0/GJ

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Step 3: Select learning rate analogues for each plant component

Plant Type & Technology	FGD	SCR	GTCC	PC boiler	LNG prod	O_2 prod
IGCC Plant						
Air separation unit						X
Gasifier area					X	
Sulfur removal/recovery	X	X				
CO_2 capture system	X	X				
CO_2 compression						
GTCC (power block)			X			

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Step 4: Estimate current capacity of major plant components

Plant Type &Technology	Current MW_{net} Equiv.
IGCC Plant Components	
Air separation units	50,000
Gasifier area	10,000
Sulfur removal/recovery	50,000
CO_2 capture system	10,000
CO_2 compression	10,000
GTCC (power block)	240,000

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Step 5: Set projection period and start of learning

Plant Type	Cumulative CCS Capacity (MW)		
	Learning Begins at:		Learning Projected to:
	1st Plant	nth Plant	
NGCC Plant	432	3,000	100,000
PC Plant	500	5,000	100,000
IGCC Plant	490	7,000	100,000
Oxyfuel Plant	500	10,000	100,000

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Step 6: Sensitivity Analysis

- Learning starts at either first or n^{th} plant
- Range of component learning rates
- Projection to 50 GW of worldwide capacity
- Lower estimates of current component capacity
- Effect of additional non-CCS experience
- Higher fuel prices for coal and natural gas
- Lower financing costs + higher plant utilization

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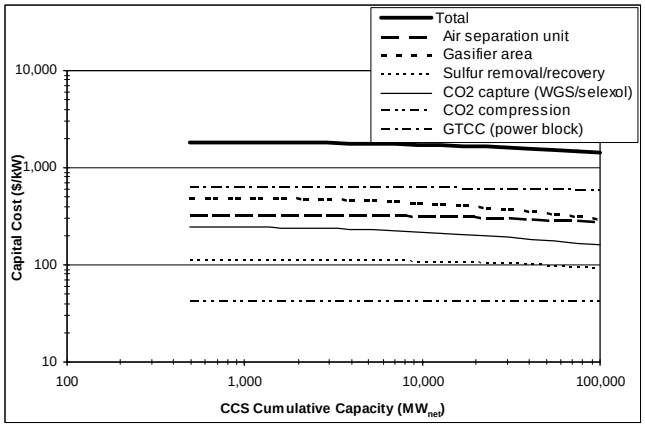
Results for IGCC Capital Cost
(Assume learning begins at first capture plant)

Based on nominal case study assumptions



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Detailed results are available in full report

NGCC Sensitivity Case	Capital Cost ($/kW)				COE ($/MWh)			
	Learning Rate	Initial Value	Final Value	% Change	Learning Rate	Initial Value	Final Value	% Change
Nominal Base Case Assumptions	0.022	916	817	10.8%	0.033	59.1	49.9	15.5%
Learning Starts with First Plant	0.014	916	811	11.5%	0.028	59.1	47.0	20.4%
Learning up to 50 GW	0.018	916	849	7.3%	0.031	59.1	52.0	12.0%
Current Capture Capacity = 0 GW	0.029	916	786	14.2%	0.037	59.1	48.8	17.4%
Non-CSS Exp. Multipliers = 2.0	0.030	916	783	14.4%	0.036	59.1	49.0	17.1%
Natural Gas Price = $6.0/GJ	0.022	925	826	10.7%	0.033	76.1	64.2	15.7%
FCF = 11%, CF = 85%	0.022	918	820	10.7%	0.034	51.6	43.3	16.1%

PC Sensitivity Case	Capital Cost ($/kW)				COE ($/MWh)			
	Learning Rate	Initial Value	Final Value	% Change	Learning Rate	Initial Value	Final Value	% Change
Nominal Base Case Assumptions	0.021	1,962	1,783	9.1%	0.035	73.4	62.8	14.4%
Learning Starts with First Plant	0.013	1,962	1,764	10.1%	0.024	73.4	60.8	17.2%
Learning up to 50 GW	0.018	1,962	1,846	5.9%	0.031	73.4	66.0	10.1%
Current Capture Capacity = 0 GW	0.026	1,962	1,744	11.1%	0.042	73.4	60.9	17.1%
Non-CSS Exp. Multipliers = 2.0	0.029	1,962	1,723	12.2%	0.068	73.4	60.4	17.8%
Coal Price = $1.5/GJ	0.021	1,965	1,786	9.1%	0.035	79.6	68.2	14.3%
FCF = 11%, CF = 85%	0.021	1,963	1,785	9.1%	0.039	57.2	48.2	15.7%

IGCC Sensitivity Case	Capital Cost ($/kW)				COE ($/MWh)			
	Learning Rate	Initial Value	Final Value	% Change	Learning Rate	Initial Value	Final Value	% Change
Nominal Base Case Assumptions	0.050	1,831	1,505	17.8%	0.049	62.6	51.5	17.7%
Learning Starts with First Plant	0.029	1,831	1,448	20.9%	0.032	62.6	48.6	22.4%
Learning up to 50 GW	0.044	1,831	1,610	12.1%	0.045	62.6	54.9	12.2%
Current Gasifier Capacity = 1 GW	0.057	1,831	1,460	20.3%	0.055	62.6	50.2	19.7%
Above + H2-GTCC = 0 GW	0.088	1,831	1,285	29.8%	0.078	62.6	45.9	26.6%
Non-CSS Exp. Multipliers = 2.0	0.062	1,831	1,432	21.8%	0.054	62.6	49.5	20.8%
Coal Price = $1.5/GJ	0.050	1,834	1,507	17.8%	0.048	68.4	56.6	17.3%
FCF = 11%, CF = 85%	0.048	1,832	1,516	17.2%	0.047	47.2	39.2	16.9%

Oxyfuel Sensitivity Case	Capital Cost ($/kW)				COE ($/MWh)			
	Learning Rate	Initial Value	Final Value	% Change	Learning Rate	Initial Value	Final Value	% Change
Nominal Base Case Assumptions	0.028	2,417	2,201	9.0%	0.030	78.8	71.2	9.6%
Learning Starts with First Plant	0.013	2,417	2,160	10.7%	0.017	78.8	68.6	12.9%
Learning up to 50 GW	0.023	2,417	2,291	5.2%	0.025	78.8	74.3	5.8%
Current Boiler Capacity = 0	0.054	2,417	2,008	16.9%	0.056	78.8	65.1	17.5%
Non-CSS Exp. Multipliers = 2.0	0.038	2,417	2,122	12.2%	0.044	78.8	68.8	12.7%
Coal Price = $1.5/GJ	0.028	2,421	2,204	9.0%	0.030	84.7	76.4	9.8%
FCF = 11%, CF = 85%	0.028	2,418	2,202	9.0%	0.031	58.8	53.0	9.9%

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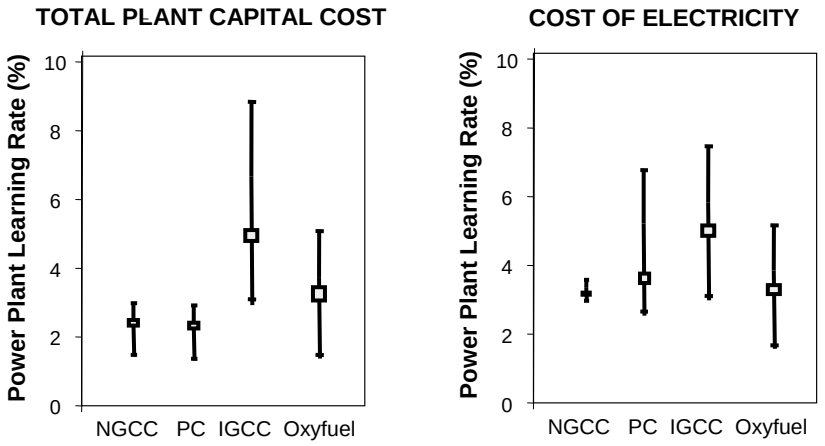
Summary of Learning Rate Results

(Based on 100 GW of cumulative CCS capacity)



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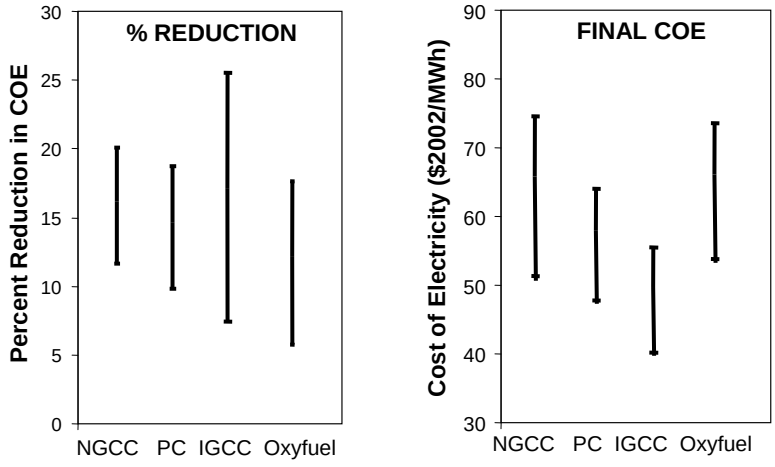
Summary of COE Results

(Based on 100 GW of cumulative CCS capacity)



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Percentage Reduction in Overall Cost of CO_2 Capture

(Based on 100 GW of cumulative CCS capacity)

Technology	Capital Cost	Cost of Capture
NGCC, post-comb	20	40
PC, post-comb	15	26
IGCC, pre-comb	15	20
Oxyfuel comb	13	13

Capture cost is the difference between plants with and without capture at any point in time. This cost falls more rapidly than the total cost of plants with capture.

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Cost of CO_2 Avoided

$/tonne CO_2 avoided relative to a SCPC plant w/o CCS

Technology	Aquifer Storage	
	Start	End
SCPC Plant	**57**	**48**
IGCC Plant	**38**	**29**

Transport + aquifer storage = $10/t CO_2 (constant)

End = 100 GW cumulative capacity

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Cost of CO_2 Avoided

$/tonne CO_2 avoided relative to a SCPC plant w/o CCS

Technology	Aquifer Storage		EOR Storage	
	Start	End	Start	End
SCPC Plant	57	48	13	4
IGCC Plant	38	29	0	-8

Transport + aquifer storage = $10/t CO_2 (constant)
Transport + EOR storage = –$15/t CO_2 (constant)
End = 100 GW cumulative capacity

Conclusions

- Future reductions in the cost of power plants with CO_2 capture will require not only sustained R&D, but also full-scale deployment to foster learning-by-doing
- Results suggests that IGCC plants with CO_2 capture have a potential for larger cost reductions compared to combustion-based plants with capture
- The timing and magnitude of future cost reductions are uncertain; policy drivers will play a key role

Caveats

- There are many!
- Please see full report for details.
  - *A spreadsheet model accompanies the report to facilitate analyses with other input assumptions*