## Report on Recent Accomplishments and Future Directions

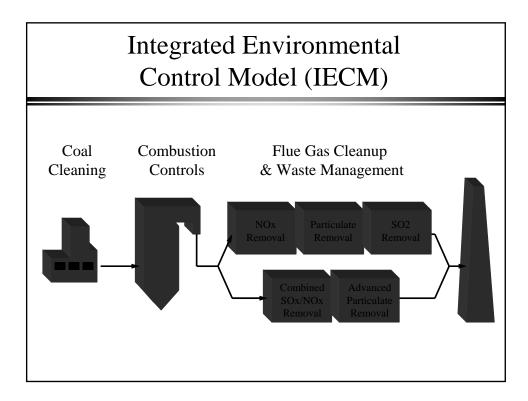
Ed Rubin, Mike Berkenpas, Urmila Diwekar, and Karen Kietzke Carnegie Mellon University and Chris Frey North Carolina State University

October 18, 1999

F	799 Projects and Funding
	nents to the Integrated Environmental Iodel (IECM)
Sponsor: Amount: COR:	Process Analysis Division \$50 k Gerst Gibbon
-	ent of a Framework for the Preliminary Id Analysis of Vision 21 Plants
Sponsor: Amount: COR:	Advanced Research & Technology Development \$150 k Gerst Gibbon (Bob Romanosky)

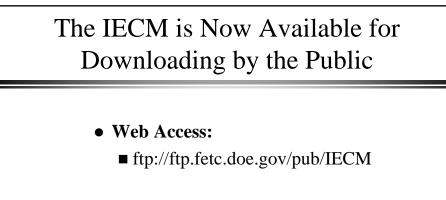
# Highlights of Activities to Date

- Completed IECM Version 3.1 plus associated technical documentation and user manuals
- Developed new performance and cost models of selected process technologies for the IECM
- Began implementing new models in the IECM code and graphical interface
- Developed a plan to add process optimization options
- Developed a conceptual framework for a Vision 21 preliminary planning model



## IECM Performance and Cost Models

- Detailed mass and energy balances, plus empirical relationships for complex process chemistry
- Calculates mass flows, energy flows, efficiency, and multi-media environmental emissions
- Component cost models (5-10 process areas per technology) explicitly linked to flowsheet performance parameters
- Calculates total capital cost, O&M costs, and COE
- Approximately 10-20 performance parameters and 10-20 cost parameters for each technology



#### • FTP Access:

- ftp.fetc.doe.gov/pub/IECM
  - anonymous login
  - any password

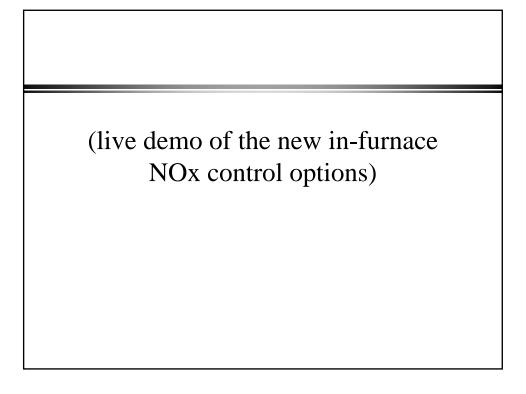
## Preliminary IECM User Group

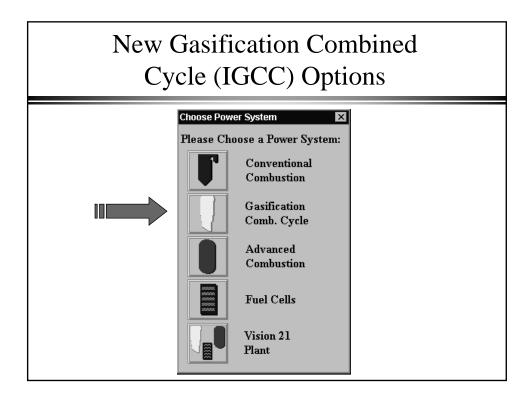
- ABB Power Plant Control
- American Electric Power
- Consol, Inc.
- Energy & Env. Research Corp.
- Exportech Company, Inc.
- FirstEnergy Corp.
- FLS Miljo A/S
- Foster Wheeler Development Corp.
- Lehigh University
- Lower Colorado River Authority
- McDermott Technology, Inc.
- Mitsui Babcock Energy Ltd.

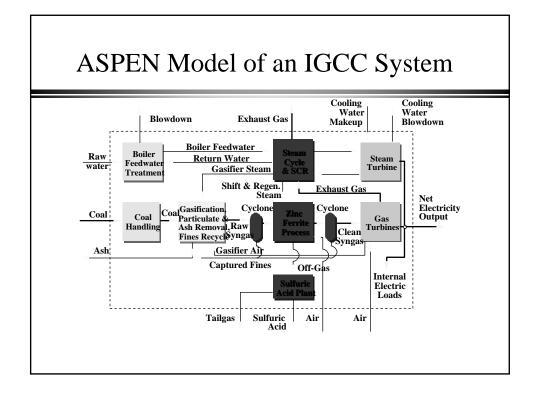
- National Power Plc.
- Niksa Energy Associates
- Pacific Corp.
- Pennsylvania Electric Association
- Potomac Electric Power Co.
- Private Consultants
- Savvy Engineering
- Sierra Pacific Power Co.
- Southern Company Services, Inc.
- Stone & Webster Engineering Corp.
- Tampa Electric Co.
- University of California, Berkeley

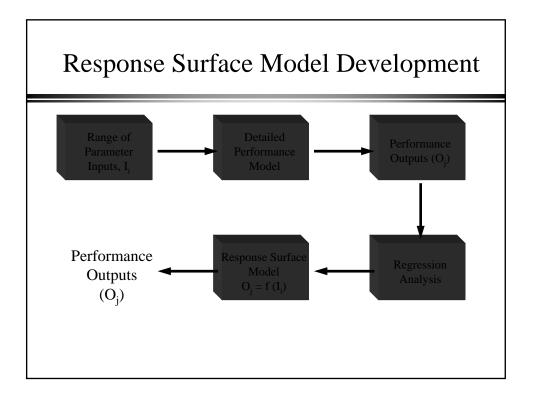
#### New Performance and Cost Models Under Development

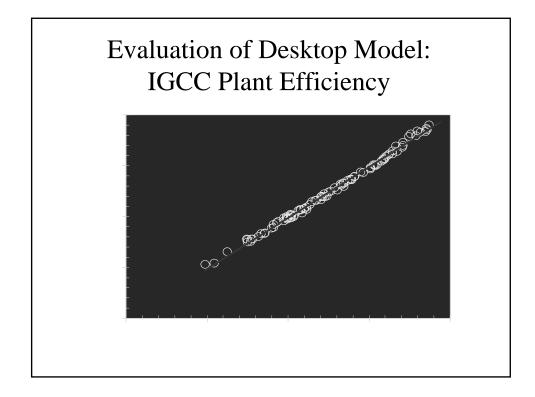
- In-Furnace NO<sub>x</sub> Controls
  - Low NOx Burners (LNB)
  - LNB + Overfire air
  - Gas Reburn
  - Selective Non-Catalytic Reduction (SNCR)
  - $\blacksquare LNB + SNCR$
  - Tangential, Wall, and Cyclone Firing
- Gasification Combined Cycle Systems
  - KRW Gasifier with Hot Gas Cleanup
  - Texaco Gasifier with Cold Gas Cleanup

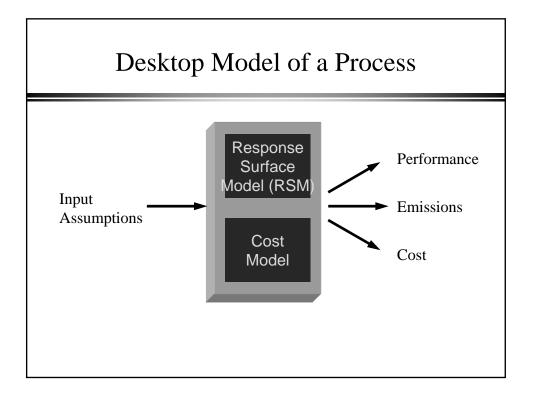






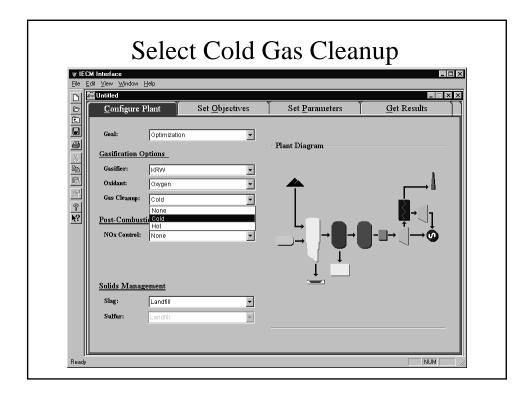




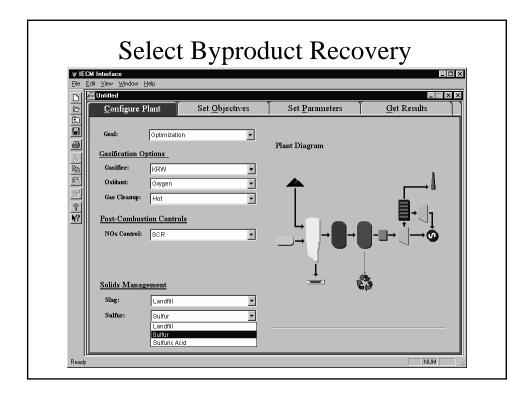


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Oxidant: KRW Lurgi			Å
Gas Cleanup: Texaco			
Post-Combustion Cont	rols		2,→√1
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Sulfur: Landfill			

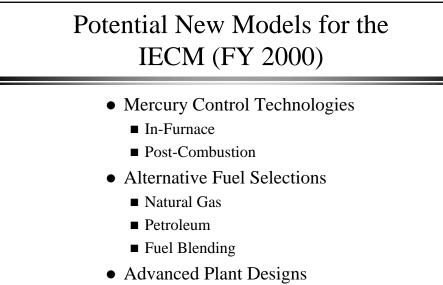
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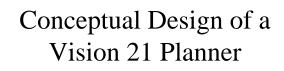
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Slag: Landfill	<b></b>		
Sulfur:			



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Over P <u>l</u> ar			ussion Istr <u>a</u> int:	Cont		Particulate Control	s <u>o</u> 2 Co	ontrol Solio
	Title	Units	Unc	Value	Calc	Min	Max	Default
1								
2		%		95.0		90.0	98.0	95.0
3		mo1 O2 / mo1 C		0.46		0.45	0.47	0.46
4	Gasifier Steam to Carbon Ratio	mol H2O / mol C		0.46	_	0.445	0.455	0.46
5		%		10.0	_	5.0	15.0	10.0
6		n %		90.0	_	80.0	95.0	90.0
7								
8					-			
9	Calcium to Sulfur Ratio	molCa/molC %		2.60		2.10	3.00	2.60
10				95.0 90.0	-	90.0 50.0	98.0 90.0	95.0 90.0
$\frac{11}{12}$		96		90.0		50.0	90.0	90.0
12	-			10.0	-	5.0	20.0	10.0
14		ppmw		10.0		2.0	20.0	10.0
15					-			
16					-			
17					-			
18								



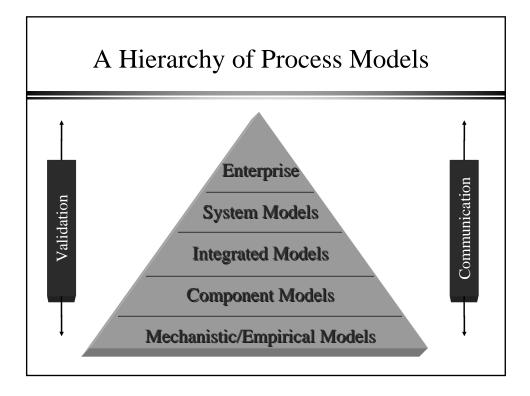
- Additional Model Parameters
- Additional Process Technologies

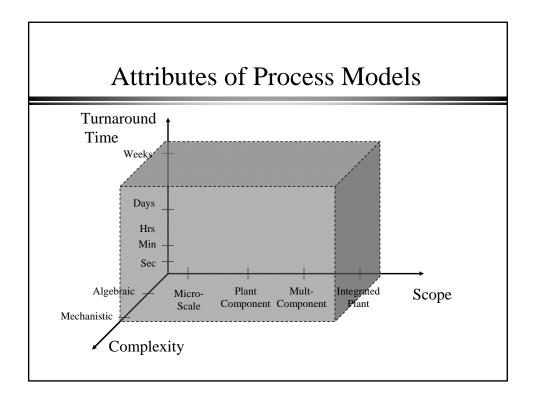


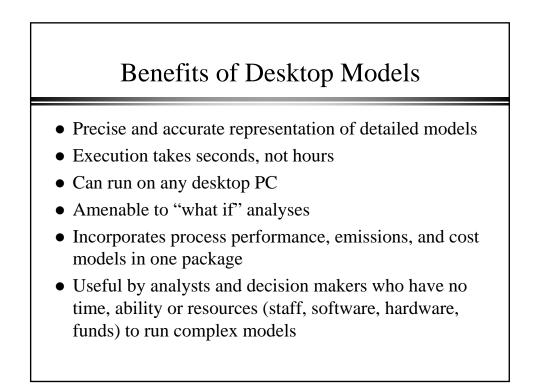
- A preliminary design model to analyze:
  - -Process Components
  - -Systems Integration
  - -Performance and Cost
  - -Process Optimization
  - -Current Uncertainties

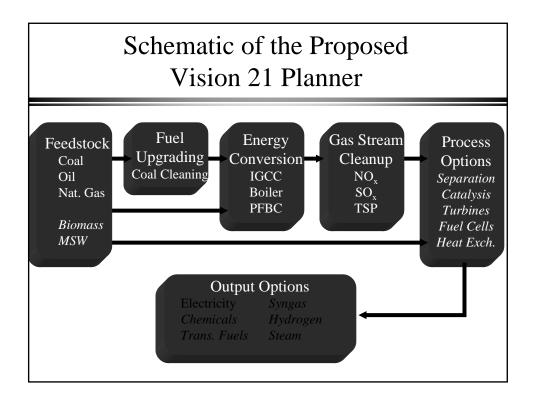
## Objectives

- Develop a flexible and easy-to-use modeling system to estimate the performance, environmental emissions and cost of a preliminary Vision 21 plant design
- Develop a framework for comparing alternative options and on a systematic basis, including effects of uncertainty

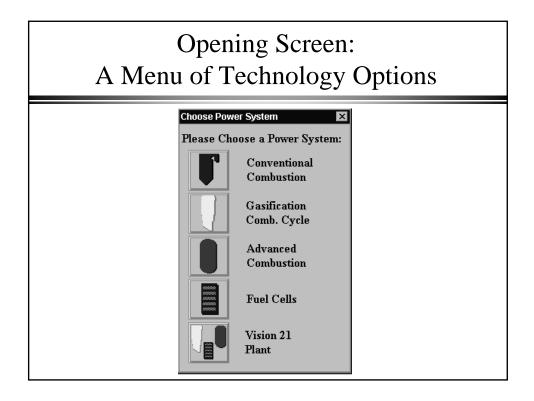


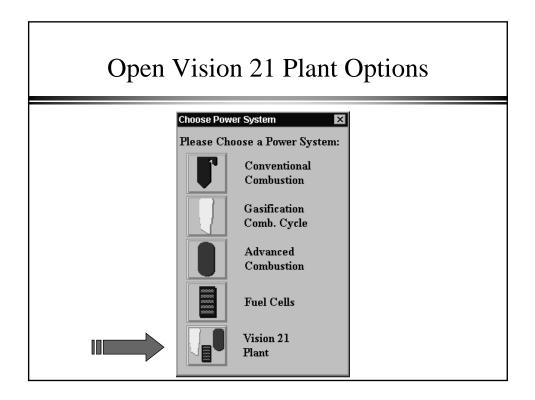


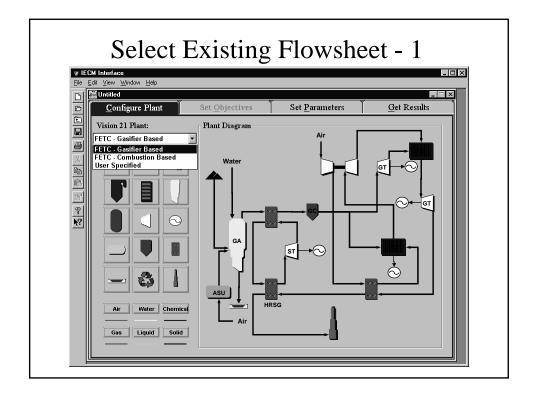


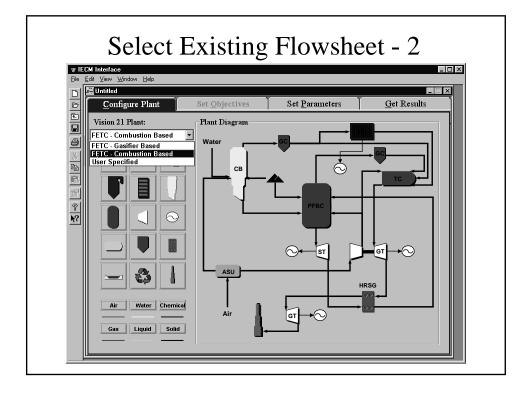




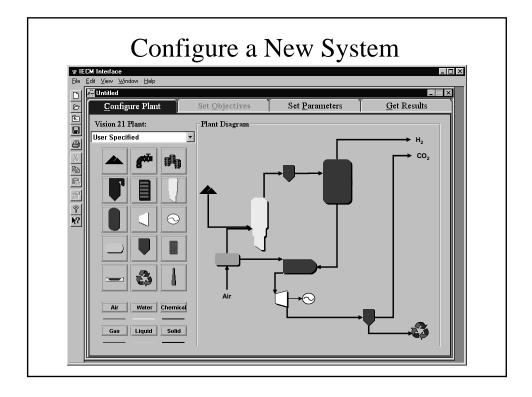






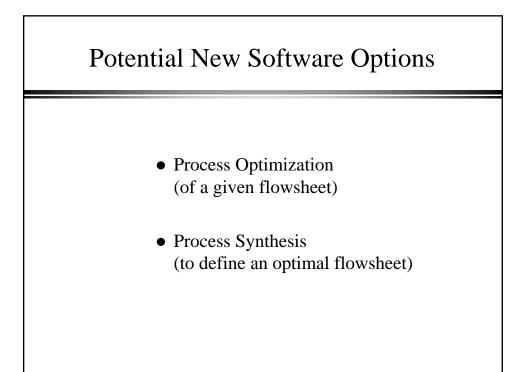


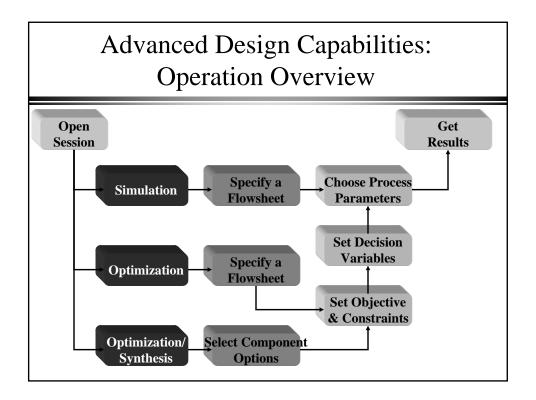


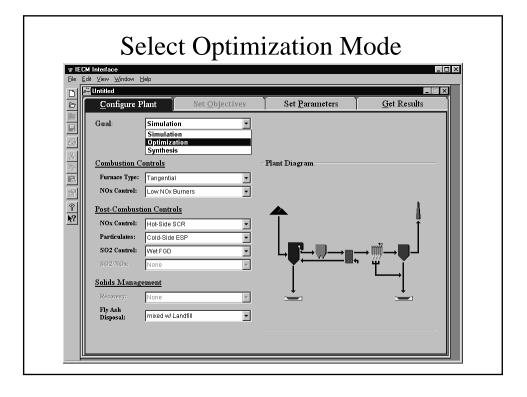


#### The Vision 21 Planner Would . . .

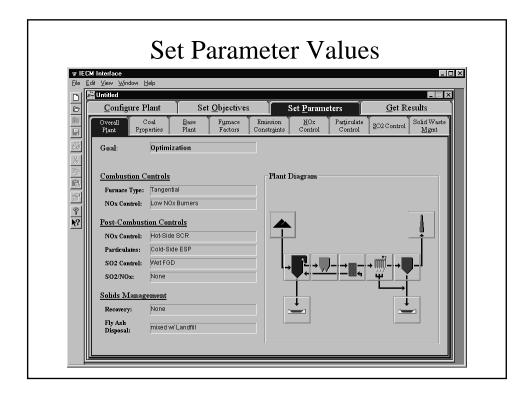
- Bring together a spectrum of performance and cost models for plant components and integrated systems, suitable for preliminary design and analysis
- Run quickly and easily on a desktop or laptop computer
- Allow new process concepts to be easily modeled
- Allow uncertainties to be characterized explicitly
- Facilitate selection of optimal (most promising) designs
- Be public domain software available to all







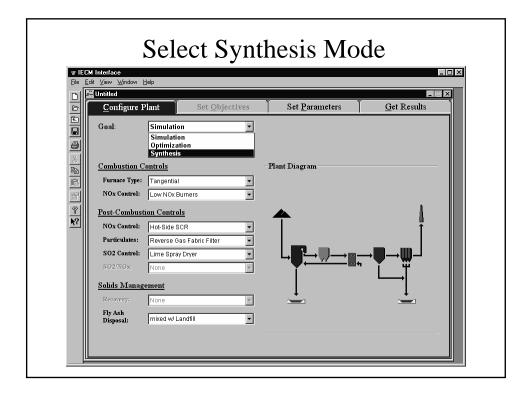
lit View Window Help					
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<u>C</u> onfigure Plant	Set Objectives	Ĭ	<u>S</u> et Pa	arameter	s <u>G</u> et Result
Objective: Minimize Capits	1 Cost 💌				
Title	Units	cv	Min	Max	
1 Emissions (Fin					
2 Particulates	lb/MBtu				
3 Nitrogen Oxides	lb/MBtu	R	0.06	0.6	
4 Sulfur Dioxide	1b/MBtu		0.1	1.2	
5 Carbon Dioxide 6 Air Toxics	lb/MBtu	1			
7 Solids Wastes	1b/MBtu 1b/MBtu	-			
8	16/MBtu				
9 Net Thermal Efficiency	Btu/kWh				
10					
11 Overall Plant Co	osts				
12 Capital Cost					
13 O&M Cost	M\$/yr				
14 Cost of Electricity	mills/kWh				
15					
16					-
17					

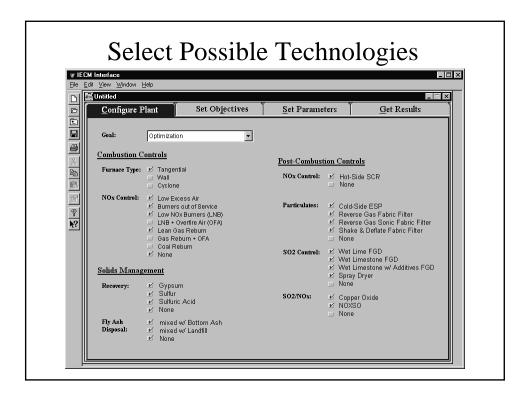


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	Overall Feedstocks		nergy iversio		s Strean leanup	n	Process Options	Co-Produ
	IGCC Cor	nventional Boiler		Fue	1 Ce11	Ĭ		PFBC
	Title	Units	Unc	Value	Calc	Min	Max	Default D
3	1 Gross Electrical Output	MWg		500		1	3000	500
3	2 Steam Cycle Heat Rate	Btu/kWh		7880		6000	11000	7880
7	3 Boiler Efficiency	%		89.21	Ľ	0	100	calc
	4 Capacity Factor	%		75		0	100	75
211111	5 Excess Air For Furnace	% stoich.		20.00	Ľ	0	40	calc
?	6 Leakage Air at Preheater	% stoich.		19.00	Ľ	0	60	calc
-	7 Gas Temp. Exiting Economizer	deg. F		700		250	1200	700
	8 Gas Temp. Exiting Air Preheater	deg. F		300		150	400	300
	9 Ambient Air Temperature	deg. F		80		-50	130	80
	10 Ambient Air Pressure	psia		14.7		12	15	14.7
	11 Ambient Air Humidity	1b H2O/1b dry air		0.018	-	0	0.03	0.018
	12 Collected Bottom Ash Solids 13 Base Plant Energy Requirement:	%		60.70	R	0	100	calc
	13 Base Plant Energy Requirement: 14 Coal Pulverizer	-		0.000	V	0	2	calc
	15 Steam Cycle Pumps	% MWg		0.6000	E	0	2	0.65
	15 Steam Cycle Pumps 16 Forced Draft Fans	% MWg % MWg		0.65		0	4	0.65
	16 Forced Draft Fans 17 Cooling System	% MWg		1.5		0	4	1.5
	17 Cooling System 18 Miscellaneous	% MWg		1.8		0	4	1.8

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		IECM Analysi	s Progress			
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		6	90.345 %	1.4e-01		
Combustion C	ontrols	7	90.462 %	2.4e-02		
Furnace Type:	Tanger	8	90.523 %	9.5e-04		
NOx Control:	Low N(	9	90.549 %	5.4e-05		
NOX CORPUT:	LOWIN	10	90.563 %	4.0e-07		
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		12	90.570 %	3.3e-09		
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302/NOX:	140116		8			
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Recovery:	None L					
Fly Ash Disposal:	mixed w/	Landfill				

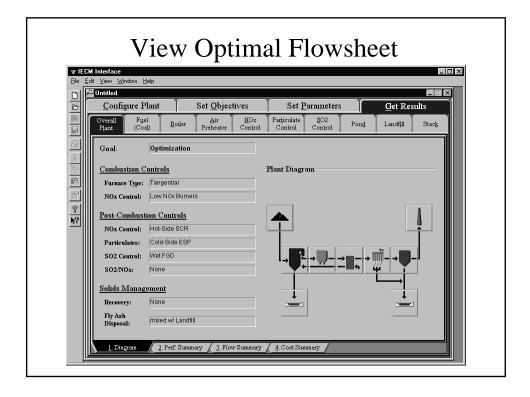
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Combustion (			[	Plant Diagra	am			
Furnace Type:	Tangential							
NOx Control:	LOW NUX BUME	irs						•
Post-Combus								
NOx Control:	Hot-Side SCR							Ť
Particulates:	Cold-Side ESP							-
SO2 Control:	Wet FGD			L→ P	→╷ノ–→		∭- <b>- </b> ↓	-1
SO2/NOx:	None							
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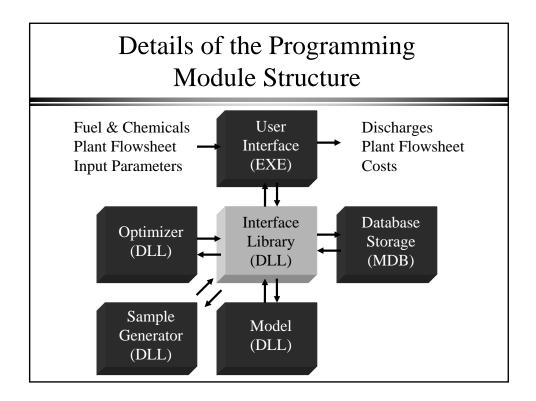


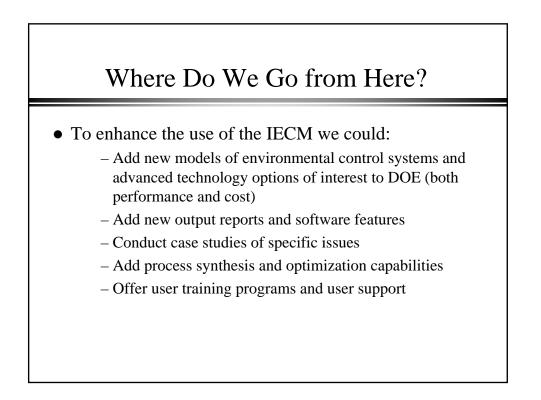


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ж.		Title		Units	Unc	Value	Calc	Min	Max	Default	DV
10	10	ross Electrical Output		MWg		500		1	3000	500	
	2 S	team Cycle Heat Rate		Btu/kWh		7880		6000	11000	7880	
	3 E	oiler Efficiency		%		89.21	V	0	100	calc	
ra <sup>1</sup>	4 C	apacity Factor		%		75		0	100	75	
?IIII	5 E	xcess Air For Furnace		% stoich.		20.00	V	0	40	calc	
<u>*?</u>	6 L	eakage Air at Preheater		% stoich.		19.00	Ľ	0	60	calc	
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	8 0	as Temp. Exiting Air Pre	heater	deg. F		300		150	400	300	
	<b>9</b> A	mbient Air Temperature		deg. F		80		-50	130	80	
		mbient Air Pressure		psia		14.7		12	15	14.7	
		mbient Air Humidity		1b H2O/1b dry air		0.018		0	0.03	0.018	
		ollected Bottom Ash So		%		60.70	R	0	100	calc	
		<u>Base Plant Energy Requ</u>	irements								
		oal Pulverizer		% MWg		0.6000	R	0	2	calc	
		team Cycle Pumps		% MWg		0.65		0	2	0.65	
		orced Draft Fans		% MWg		1.5		0	4	1.5	
	17 0	ooling System		% MWg		1.8 1.3		0	2	1.8	
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Combustion Con	trols	6	787.3	1.4e-01		
	anger	7	702.0	2.4e-02		
		8	669.8	9.5e-04		
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Fly Ash Disposal:	nixed w/ Lar	dfill				







#### Where Do We Go from Here?

- To develop the Vision 21 Planner we would:
  - Implement preliminary versions of enabling technology models (both performance and cost)
  - Use the Vision 21 Planner as a testbed for systems integration development
  - Add process synthesis and optimization capabilities
  - Incorporate dynamics modeling of integrated systems
  - Develop linkages to more detailed models of process components and systems (modeling hierarchy)