The Integrated Environmental Control Model (IECM)

#### Ed Rubin, Mike Berkenpas and Karen Kietzke

### Center for Energy and Environmental Studies Carnegie Mellon University

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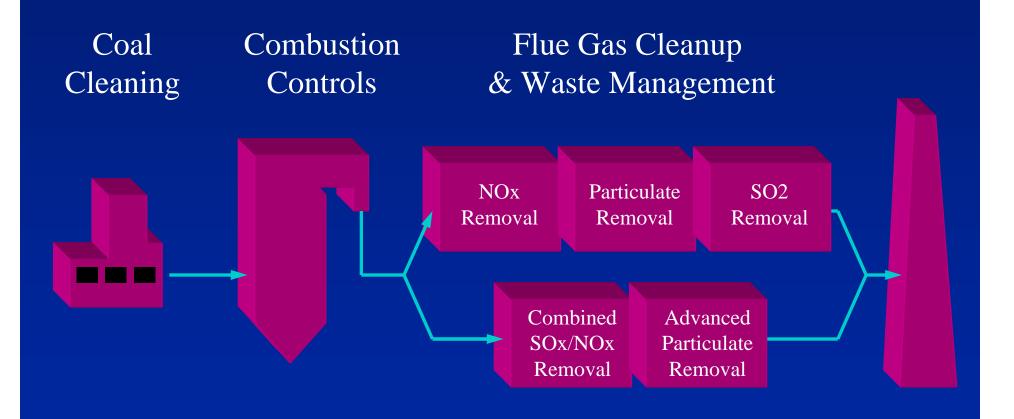
### Objectives

- Develop reliable and easy-to-use models to estimate the environmental performance and cost of conventional and advanced technologies to produce electricity from coal
- Develop a framework for comparing alternative options on a systematic basis, including the effects of uncertainty

### Approach

Process Technology Models
Engineering Economic Models
Advanced Software Capabilities
Systems Analysis Framework

Integrated Environmental Control Model (IECM)



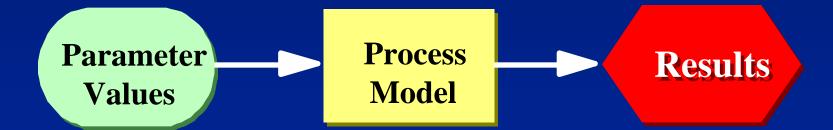
### Process Performance Models

- Employ detailed mass and energy balances
- Empirical relationships and models used for complex process chemistry
- Calculate component and system mass flows, energy flows, and efficiency
- Calculate multi-media environmental emissions
- Approximately 10-20 performance parameters for each process technology

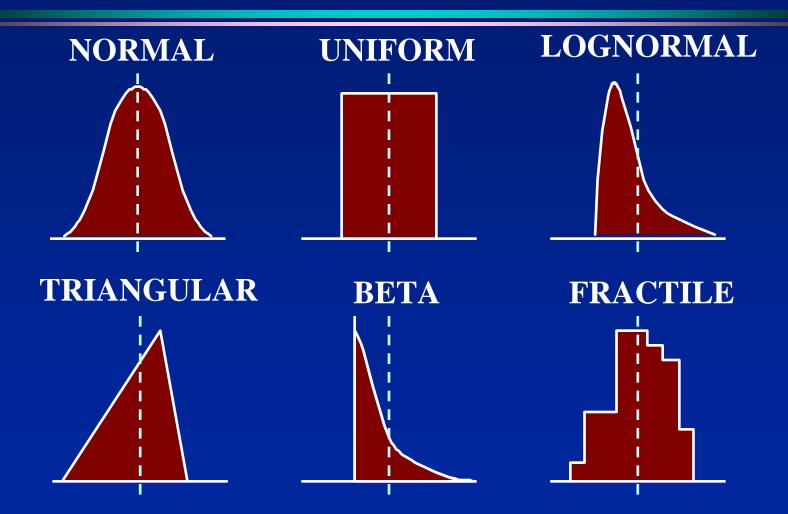
### Process Cost Models

- Direct cost models for each major process area (typically 5-10 areas per technology)
- Explicit links to process performance models
- Calculate total capital cost
- Calculate variable operating costs
- Calculate fixed operating costs
- Calculate annualized cost of electricity
- Approximately 20-30 cost parameters for each process technology

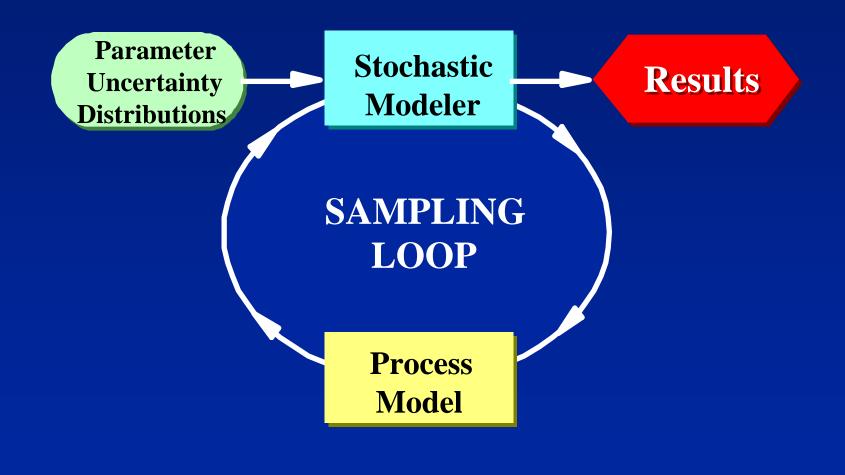
# Conventional Process Modeling (Deterministic Simulation)



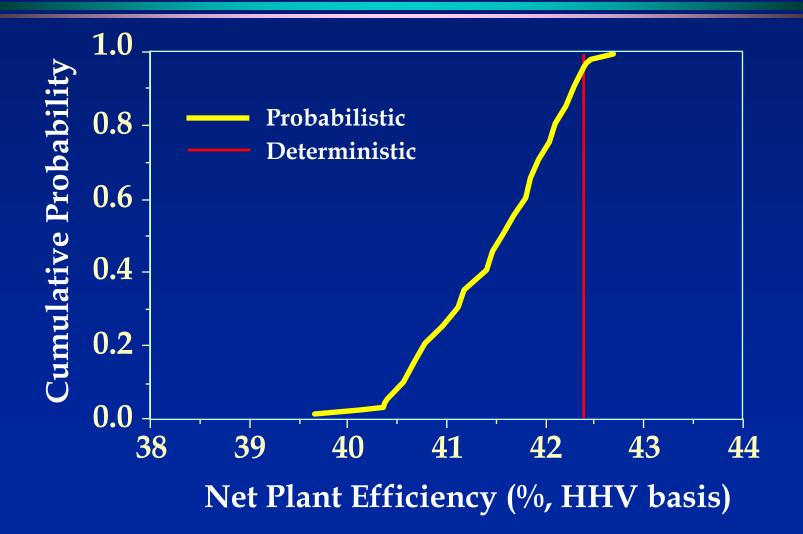
# Parameter Uncertainty Distributions



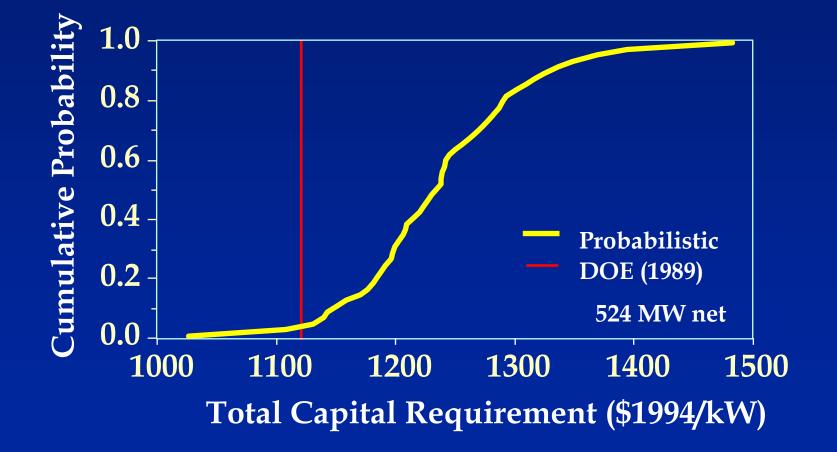
### **Stochastic Simulation**

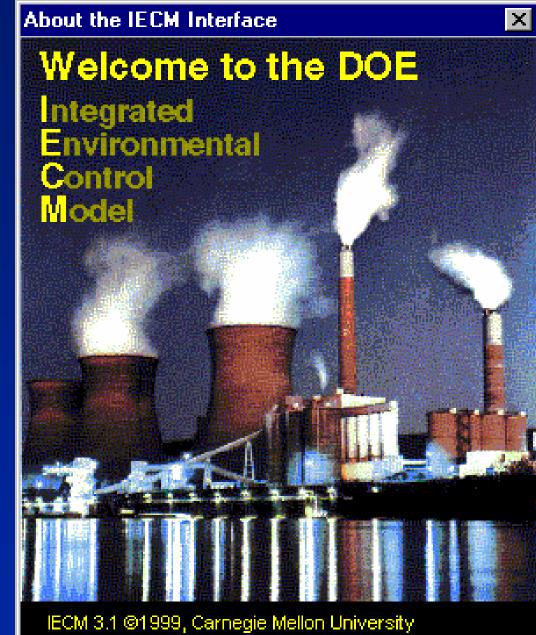


### Calculated Plant Efficiency



### Total Plant Capital Cost





IECM Interface 3.1 ©1999, Carnegie Mellon University

# (live demo of the IECM)

# The IECM is Now Available for Downloading by the Public

Web Access:
ftp://ftp.fetc.doe.gov/pub/IECM

FTP Access:
 ftp.fetc.doe.gov/pub/IECM

 anonymous login
 any password

### Additional Technology Options

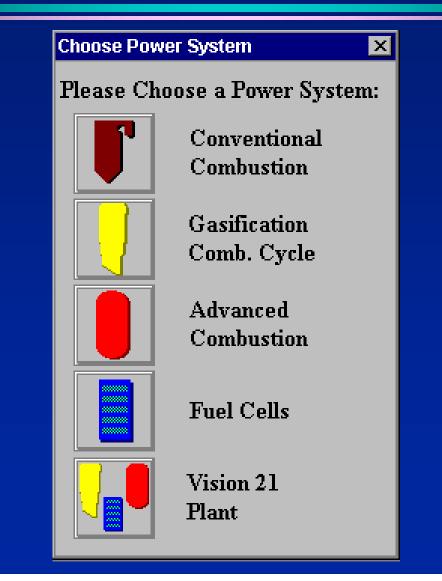
### • Planned

- Combustion NO<sub>x</sub> Controls
  - Selective Non-Catalytic Reduction (SNCR)
  - Low NOx Burners
  - Overfire air
  - Low Excess Air
  - Lean Gas Reburn
  - Burners Out of Service
  - Selected combinations of the above

### • Proposed

- Post-Combustion Controls
  - Air Toxics (mercury)
- Other Fuels
  - Natural Gas
  - Petroleum
  - Fuel Blending
- Alternative Power Generation Systems

# Future Development: A Menu of Technology Options



# Select Gasification Combined Cycle (IGCC) Options

Choose Powe	er System 🔀	
Please Cho	oose a Power System:	
	Conventional Combustion	
	Gasification Comb. Cycle	
	Advanced Combustion	
	Fuel Cells	
	Vision 21 Plant	

## Select KRW Gasifier

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# Select Oxygen Plant

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	Configure Plant         Goal:       Optimit         Gasification Options         Gasifier:       KRW         Oxidant:       Oxyget         Gas Cleanup:       Air         Oxyget       Oxyget         Post-Combustion Con       None         NOx Control:       None         Solids Management       Slag:         Landfil       Sulfur:       Landfil	zation	Plant Diagram	
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### Select Cold Gas Cleanup

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	Goal:	Optimizatio	on 💌		
		. ·		- Plant Diagram	
X	Gasification O	<u>ptions</u>		-	
*	Gasifier:	KRW	-		
C.	Oxidant:	Oxygen	•		
ď	Gas Cleanup:				
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<b>%</b> <b>∖</b> ?	Post-Combust	Cold			_ 【] │
	NOx Control:	Hot			
	NOX COREGI.	None	<b>_</b>		
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	Solids Manag	ement			
	Slag:	Landfill	•		
	Sulfur:	Landfill	<b>v</b>		
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# Select NO<sub>x</sub> Control

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	Goal: <u>Gasification O</u> Gasifier: Oxidant:	Optimization <b>ptions</b> KRW Oxygen	n 💌	Plant Diagram	
	Gas Cleanup:	Cold			
* *?	<u>Post-Combust</u> NOx Control:	SCR	<u> </u>		┛┑ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙ ┙
		None SCR			
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	Slag:	Landfill	-		
	Sulfur:	Landfill	Y		
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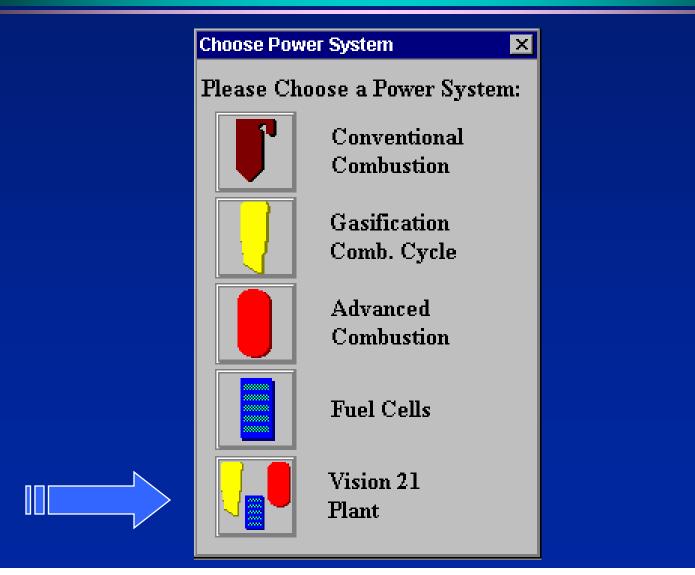
# Select Byproduct Recovery

😻 IECM Interface	
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	<u>G</u> et Results
Configure Plant       Set Objectives       Set Parameters         Image: Goal:       Optimization       Image: Plant Diagram	
B Plant Diagram	
S Gasification Options	
Gasification Options       Gasifier:     KRW	
Oxygen 🗸 🛆	
Gas Cleanup: Hot	
?     Post-Combustion Controls	
<u>Post-Combustion Controls</u>	
NOx Control: SCR 🔽	l- <b>-</b> →ḋ→ፙ
Solids Management	
Slag: Landfill	
Sulfur: Sulfur	
Sulfur Sulfuric Acid	
Ready	

### Set Process Parameters

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9				Title	Units		Unc	Value	Calc	Min	Max	Default	DV
8			1	<u>Gasifier Design</u>									
8			2	Gasifier Carbon Conversion	%			95.0		90.0	98.0	95.0	
			3	Gasifier Oxygen to Carbon Ratio	mo1O2/m	olC		0.46		0.45	0.47	0.46	
			4	Gasifier Steam to Carbon Ratio	mo1 H2O / n	101 C		0.46		0.445	0.455	0.46	
			5	Coal-bound N Converted to NH3	%			10.0		5.0	15.0	10.0	
?			6	Sulfur Retained in Gasifier Bot Ash	1 %			90.0		80.0	95.0	90.0	
▶?			7										
<u>~</u>			8	Emissions Control									
			9	Calcium to Sulfur Ratio	molCa/m	olC		2.60		2.10	3.00	2.60	
		1	_	Sulfation Unit Conversion	%			95.0		90.0	98.0	95.0	
			_	NH3 Converted to NOx in Turbine	%			90.0		50.0	90.0	90.0	III
		.		SCR NOx Removal Efficiency	%			80.0		50.0	90.0	80.0	_
				SCR NH3 Slip	ppmw			10.0		5.0	20.0	10.0	_
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### Open Vision 21 Plant Options

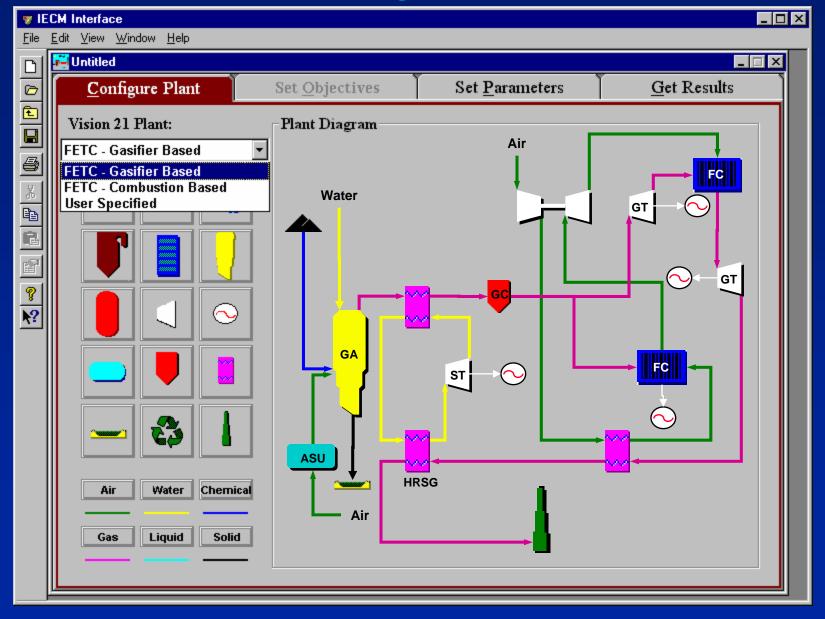


# Welcome to the Vision 21 Planner

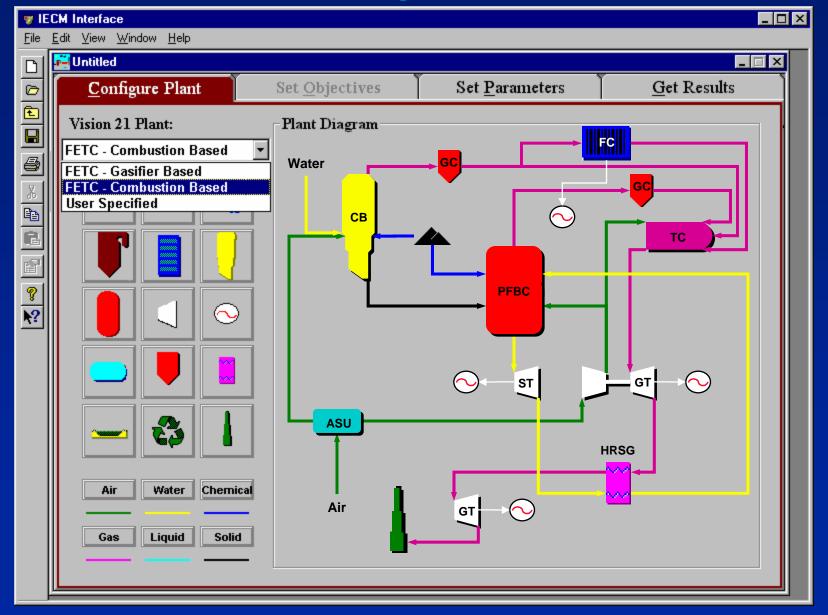
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## Select Existing Flowsheet - 1



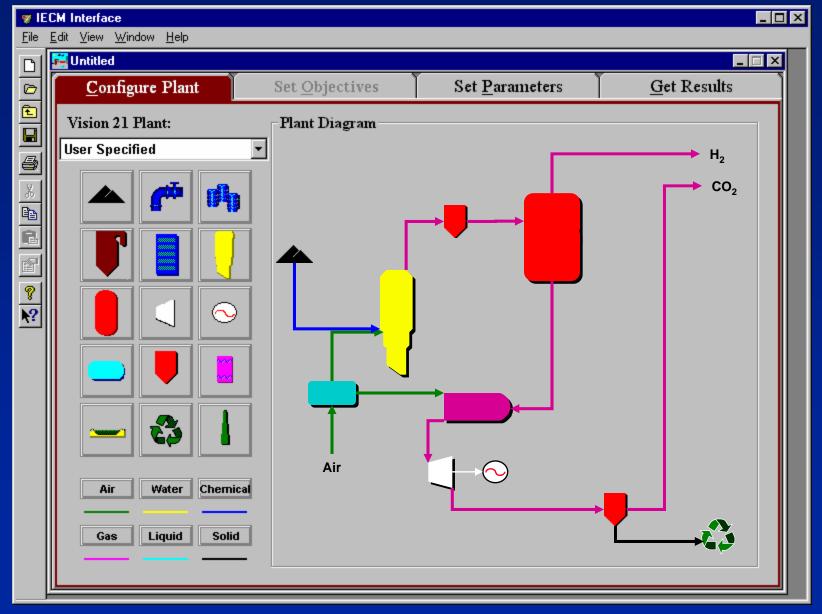
## Select Existing Flowsheet - 2



## Vision 21 Workbench

	CM Interface			
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	Air Water Chem	ical		
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	Gas Liquid Soli	d		
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## Configure a New System

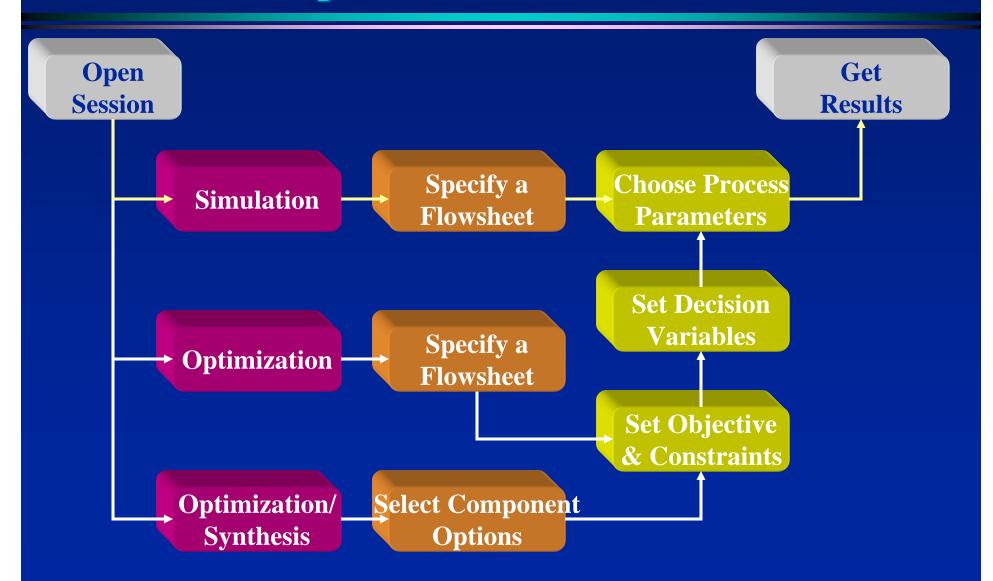


### Potential New Software Options

• Process Optimization

• Process (Flowsheet) Synthesis

# Advanced Design Capabilities: Operation Overview



# Select Optimization Mode

*		Interface				
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6	Ir	<u>C</u> onfigure P	lant 🔰 Set 🤇	<u>)</u> bjectives	Set <u>P</u> arameters	<u>G</u> et Results
		Goal:	Simulation Simulation Optimization Synthesis	<b>•</b>		
8 1		Combustion Co			Plant Diagram	
		Furnace Type:	Tangential	•		
đ		NOx Control:	Low NOx Burners	•		
?		<u>Post-Combusti</u>	on Controls		4	
?		NOx Control:	Hot-Side SCR	-		T II
		Particulates:	Cold-Side ESP	-		
		SO2 Control:	Wet FGD	-	· L <mark>I</mark> →U→ <sup>∞</sup> -	→▥ਁ→■┘ │║
		SO2/NOx:	None	7	₩←_₩←₩♦	י יי די וו
		<u>Solids Manage</u>	ment			
		Recovery:	None	~	· · · · · · · · · · · · · · · · · · ·	· · · · · ·
		Fly Ash Disposal:	mixed w/ Landfill	•		

## Set Objective and Constraints

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ile <u>E</u>	<u>i</u> dit <u>V</u> iew <u>W</u>	indow <u>H</u> elp					
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	<u>C</u> onfi	gure Plant Set Obj	ectives	Ĩ	<u>S</u> et Pa	rameters	<u>G</u> et Results
	Objectiv	e: Minimize Capital Cost	•				
		Title	Units	cv	Min	Max	
	1	Emissions (Final)					
I	2	Particulates	lb/MBtu				
I	3	Nitrogen Oxides	lb/MBtu	V	0.06	0.6	
Ш	4	Sulfur Dioxide	1b/MBtu	V	0.1	1.2	
II	5	Carbon Dioxide	1b/MBtu				
II	6	Air Toxics	1b/MBtu				
I	7	Solids Wastes	lb/MBtu				
I	8						
I	9	Net Thermal Efficiency	Btu/kWh				
I	10						
I	11						
Ш	12		M\$				
l	13		M\$/yr				
I	14	-	mills/kWh				
l	15						
Ш	16						
Ш	17						
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## Set Parameter Values

	<u>C</u> onfigure P	lant 🗍	Set	<u>O</u> bjectives	;	Set 1	<u>P</u> aramet	ers	<u>G</u> et Re	esults
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	Goal:	Optimizatio	n							
	Combustion C	ontrols			⊢ Pl₂	unt Diag	ram			
	<b>Furnace Type:</b>	Tangential			_					
	Furnace Type:     Tangential       NOx Control:     Low NOx Burners			-						
	Post-Combust	ion Controls	L							
	NOx Control:	Hot-Side SCI	२			₽.				<b>-</b>
	Particulates:	Cold-Side ES	)P							_
I	SO2 Control:	Wet FGD				l_ ĵ	L → ,,).	- <mark>→</mark>	→ , ,	J_I ∣
	SO2/NOx:	None					< <u>···</u>		<u> </u>	
	Solids Manage	ement					_			_
	Recovery: None					3			· · · · · · · · · · · · · · · · · · ·	
	Fly Ash Disposal:	mixed w/ Lan	dfill							

# Select Decision Variables

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	<u>C</u> onfigure Plant Set				<u>O</u> bjectiv	es		Set <u>P</u> ar	amet	ers	<u> </u>	et Resul	lts	
	Heedstocks			Fuel ograde		nergy versio		s Strean leanup	n	Process Options	Co-P	roducts		
S C		IGCC Conv			entional Boi	iler		Fuel	Ce11			PFBC		
Å			Title		Univ	ts	Unc	Value	Calc	Min	Max	Default	DV	
8	1		ectrical Output	:	MW	/g		500		1	3000	500		
C.	2	Steam Cy	ycle Heat Rate		Btu/k	Wh		7880		6000	11000	7880		
	3	Boiler Eff	ficiency		%			89.21	K	0	100	calc		
P	4	Capacity	Factor		%			75		0	100	75		
8	5	Excess A	hir For Furnace	•	% sto	ich.		20.00		0	40	calc		
<b>N</b> ?	6	Leakage	Air at Preheat	er	% sto	ich.		19.00		0	60	calc		
	7	Gas Tem	p. Exiting Ecor	nomizer	deg.	F		700		250	1200	700		
	8	-	p. Exiting Air I		deg.	F		300		150	400	300		
	9		Air Temperati	ure	deg.	F		80		-50	130	80		
	10	Ambient	Air Pressure		psi	a		14.7		12	15	14.7		
	11	Ambient	Air Humidity		16 H2O/16	dry air		0.018		0	0.03	0.018		
	12		d Bottom Ash		%			60.70	M	0	100	calc		
	13		lant Energy Re	quirements										
	14	Forced Draft Fans		% MV			0.6000		0	2	calc			
	15			% MV	-		0.65		0	2	0.65			
	16			% MV			1.5		0	4	1.5			
	17	Cooling System			% MV			1.8		0	2	1.8		
	18	Miscella	neous		% MV	Wg		1.3		0	4	1.3		
	1	Performan	nce <u>2</u> . F.	inancing /	<u>3</u> . Retrof	it Cost	<u> </u>	<u>4</u> . Capital Co:	st /	<u>5</u> .0&M	Cost <u>6</u> .	O&M Esc	alation/	

### Get Results (Run Model)

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lli	_ ~		IECM Analysis			×	_	
	Overall F <u>u</u> el Plant (Coal)				. 4	Landf <u>i</u> ll Stac <u>k</u>	I	
		<u> </u>	IECM Analysis	s Progress	<u> </u>		al	
	Goal:	Optim	Iteration	Obj. Function Value	Optimizer Error Value			
			6	90.345 %	1.4e-01			
	Combustion C	ontrols	7	90.462 %	2.4e-02			
	Furnace Type:	Tanger	8	90.523 %	9.5e-04			
	NOx Control:	Low N(	9	90.549 %	5.4e-05			
		20111	10	90.563 %	4.0e-07			Ш
	Post-Combust		11	90.568 %	1.7e-07			
			12	90.570 %	3.3e-09			
	NOx Control:	Hot-Sic	13	90.570 %	6.2e-11			
	Particulates:	Cold-S						
	SO2 Control:	Wet FG					.,,	
I	SO2/NOx:	None		Calculating New Decis:	ion Variables		Ψ	
	Solids Manag Recovery:	ement None			Pause Sto	p		
	Fly Ash Disposal:							
	<u>1</u> . Diagram	<u>2</u> . Per	f. Summary 🖌	3. Flow Summary	4. Cost Summary /			1

### View Results

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₩ 8		Goal:	Optimization							
è		Combustion C	ontrols		Г	Plant Diagr	am			
		Furnace Type:	Tangential							
8		NOx Control:	Low NOx Burne	rs						
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<u> </u>		NOx Control:	Hot-Side SCR							
		Particulates:	Cold-Side ESP							
		SO2 Control:	Wet FGD			_ <u> </u> _1	- → ,,	→ <mark>~~</mark> — → 🚺	∭→	_J 📗
		SO2/NOx:	None						ř T	
		Solids Manage	ement				1			-
		Recovery:	None							2
		Fly Ash Disposal:	mixed w/ Landfi	II						
		<u>1</u> . Diagram	2. Perf. Summ	ary 🖌 <u>3</u> . Flow	Summary	4. Cost Sur	nmary /			

# Select Synthesis Mode

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		Goal:	Simulation Simulation Optimization		
*		<u>Combustion</u> C	Synthesis Controls	Plant Diagram	
		Furnace Type:	Tangential 🗨		
ď		NOx Control:	Low NOx Burners		
?		Post-Combust	tion Controls		
▶?		NOx Control:	Hot-Side SCR		<b>↑</b>
		Particulates:	Reverse Gas Fabric Filter 📃		
		SO2 Control:	Lime Spray Dryer		<b>→●</b> → <b>●</b> →
		SO2/NOx:	None		"ĭ."
		Solids Manag	ement		
		Recovery:	None	· · · · · · · · · · · · · · · · · · ·	<u> </u>
		Fly Ash Disposal:	mixed w/ Landfill		

### Select Possible Technologies

IECM Interface				
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	Set Objectives	<u>S</u> et Parame	ters	Get Results
Configure Plant Goal: Optim Combustion Control Furnace Type: V Ta W Furnace Type: V Ta W V C NOx Control: V L V B V V C NOx Control: V L V V C V NOX Control: V L C V NOX Control: V L C V V C V V C V V C V V C V V C V V V C V V V C V V V V C V	nization  Is  angential (all yclone ow Excess Air urners out of Service ow NOx Burners (LNB) NB + Overfire Air (OFA) ean Gas Reburn as Reburn + OFA oal Reburn one  t Sypsum Gulfur Sulfur Sulfuric Acid	<u>Set Paramet</u> <u>Post-Combust</u> NOx Control: Particulates: SO2 Control: SO2/NOx:	ion Con ✓ Hot □ Nor ✓ Colo ✓ Rev ✓ Rev ✓ Sha □ Nor ✓ Wet ✓ Wet ✓ Wet ✓ Spr: □ Non	Atrols Side SCR The d-Side ESP rerse Gas Fabric Filter rerse Gas Sonic Fabric Filter ake & Deflate Fabric Filter t Lime FGD t Limestone FGD t Limestone W/ Additives FGD ay Dryer te oper Oxide XSO

### Set Parameters

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Ø		<u>C</u>	onfigure	: Plant	Set	<u>O</u> bjectiv	es		Set <u>P</u> ar	amet	ers	<u> </u>	et Resul	lts	
			verall lant	Feedstoc	ve l	Fuel ograde	Et Con	nergy versio	Gas Stream on Cleanup			Process Options Co-Products			
	I,		IGC	с	Conv	entional Bo	iler		Fuel	l Cell			PFBC		
Å				Title		Uni	ts	Unc	Value	Calc	Min	Max	Default	DV	
	Ш	1	Gross El	ectrical Output	:	MM	/g		500		1	3000	500		
	Ш	2	Steam C	ycle Heat Rate		Btu/k	Wh		7880		6000	11000	7880		
	Ш	3	Boiler Ef	ficiency		%			89.21	M	0	100	calc		
đ	Ш	4	Capacity	7 Factor		%			75		0	100	75		
8	Ш	5	Excess A	Air For Furnace	<b>1</b>	% sto	ich.		20.00		0	40	calc		
<b>N</b> ?	Ш	6	Leakage	Air at Preheat	er	% sto	ich.		19.00	N	0	60	calc		
<u> </u>	Ш	7	Gas Tem	Gas Temp. Exiting Econom		nomizer deg. F			700		250	1200	700		
	Ш	8	Gas Tem	up. Exiting Air I	Preheater deg. F		F		300		150	400	300		
	Ш	9	Ambient	t Air Temperati	ure	deg. F			80		-50	130	80		
	Ш	10	Ambient	t Air Pressure		psi	a		14.7		12	15	14.7		
	Ш	11	Ambient	t Air Humidity		16 H2O/16	) dry air		0.018		0	0.03	0.018		
	Ш	12	Collecte	d Bottom Ash	Solids	%			60.70		0	100	calc		
	Ш	13	_	<u>lant Energy Re</u>	<u>quirements</u>										
	Ш	14	Coal Pul	verizer		% M'	Wg		0.6000	M	0	2	calc		
		15	-	ycle Pumps		% M'	Wg		0.65		0	2	0.65		
		16	Forced I	Oraft Fans		% M'	Wg		1.5		0	4	1.5		
		17		-		% M'	Wg		1.8		0	2	1.8		
		18	Miscella	meous		% M'	Wg		1.3		0	4	1.3		
		1	Performar	nce <u>2</u> . F	inancing /	<u>3</u> . Retrof	ñt Cost	<u> </u>	<u>l</u> . Capital Cos	st /	<u>5</u> .0&M	:Cost <u>6</u> .	.O&M Esc	alation/	7

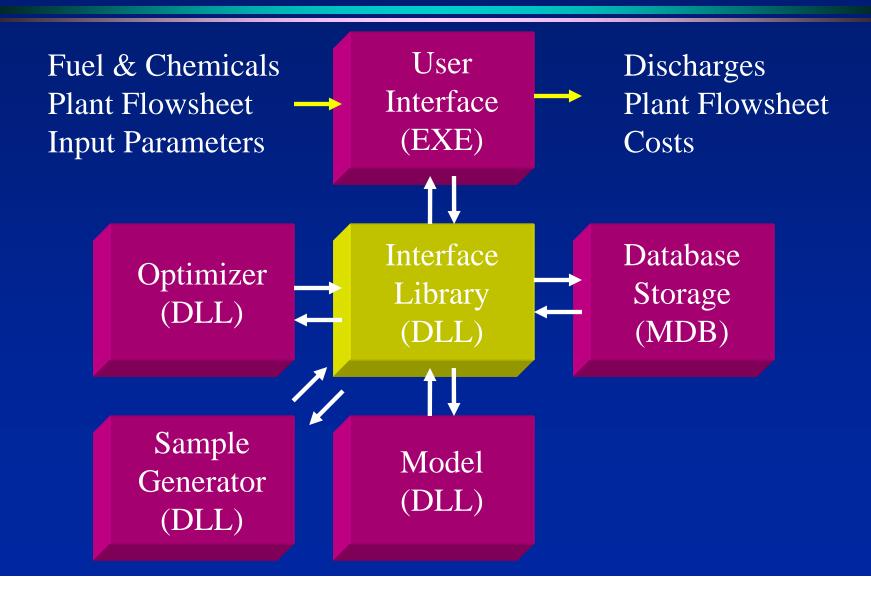
## Get Results (Run Model)

	M Interface								_ [				
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II.	<u>C</u> onfigure P	lant	Set <u>(</u>	<u>D</u> bjectives	Set <u>P</u>	arameters		sults					
	Overall Fue Plant (Coa	ŋ)   <mark>臣</mark>	Diller Preh	<u>a</u> ir <u>N</u> Ox leater Control	Par <u>t</u> iculate Control	<u>S</u> O2 Control	Pon <u>d</u>	Landf <u>i</u> ll	Stac <u>k</u>				
	Goal:	Optim	IECM Analysis	s Progress			×						
II			Iteration	Obj. Function Value	e Optimizer	Error Value							
	Combustion C	ontrols	6	787.3		4e-01							
	<b>Furnace Type:</b>	Tanger	7	702.0		4e-02							
			8	669.8		Se-04							
II	NOx Control:	Low N(	9	619.3 627.5		4e-05 De-07							
II	Best Combust	Post-Combustion Cor		580.5		0e-07 7e-07			1				
II			11	526.2		3.3e-09							
	NOx Control:	Hot-Sic	13	526.2		2e-11		L	<u>+</u> ∥				
	Particulates:	Cold-S											
	SO2 Control:	Wet FG						→∭→					
	SO2/NOx:	None		Calculating New Dec	ision Variables			Ψ					
Solids Management													
	Recovery:	None											
	Fly Ash Disposal:	mixed w/	Landfill										
	<u>1</u> . Diagram	<u>2</u> . Perf	Summary /	3. Flow Summary /	4. Cost Sur	nmary /							

# View Optimal Flowsheet

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<u>C</u> onfigure Pl	lant T	Set <u>O</u> bject	ives	Set <u>I</u>	2 arameters	;	<u>G</u> et Res	
Overail Fuel Plant (Coa		<u>A</u> ir Preheater	<u>N</u> Ox Control	Par <u>t</u> iculate Control	<u>S</u> O2 Control	Pon <u>d</u>	Landf <u>i</u> ll	Stac <u>k</u>
Goal:	Optimization							
Combustion C	ontrols		Г	Plant Diagr	am			
Furnace Type:	Tangential							
NOx Control:	Low NOx Burne	rs						
Post-Combusti	ion Controls							
NOx Control:	Hot-Side SCR							<b>₹</b>
Particulates:	Cold-Side ESP							
SO2 Control:	Wet FGD			l , ŀ	- →,,,,	+ <mark>~~</mark> +∭	∭- →	-1
SO2/NOx:	None						<u> </u>	
Solids Manage	ement				1			
Recovery:	None							1
Fly Ash Disposal:	mixed w/ Landfi	II						
<u>1</u> . Diagram	2. Perf. Sumn	ary <u>3</u> . Flow	Summary	/ <u>4</u> . Cost Sur	nmary /			

# IECM Programming Module Structure



### Model Applications

- Process design
- Technology evaluation
- Cost estimation
- R&D management

- Risk analysis
- Environmental compliance
- Marketing studies
- Strategic planning

### Please let us know what you think

rubin@cmu.edu mikeb@cmu.edu